



# Comprehensive kinetic study on ammonia/ethylene counter-flow diffusion flames: influences of diluents

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## Abstract

This study aimed to investigate the effects of ammonia addition on ethylene counter-flow diffusion flames with different diluents on the fuel or oxidizer side, using kinetic analyses. A special emphasis was put on assessing the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> on C<sub>2</sub>H<sub>4</sub> combustion chemistry. The chemical effects could be evaluated by comparing fictitious inert NH<sub>3</sub> or CO<sub>2</sub> with normal active NH<sub>3</sub> or CO<sub>2</sub>. The results revealed that the addition of NH<sub>3</sub> decreased the mole fractions and production rates of key soot precursors, such as acetylene, propynyl, and benzene. When CO<sub>2</sub> was used as the dilution gas, the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> were affected by the chemical effects of CO<sub>2</sub> to varying degrees. With the oxidizer-side CO<sub>2</sub> addition, the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> reduced the mole fractions of H, O, OH radicals, acetylene, propynyl, and benzene, while the effects differed from the fuel-side CO<sub>2</sub> addition. The coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> also promoted the formation of aldehyde contaminants, such as acetaldehyde, to some extent, particularly with CO<sub>2</sub> addition on the oxidizer side.

**Keywords** Ammonia addition · Diluents · Coupled chemical effects · Kinetic analysis

## 1 Introduction

The goal of reducing carbon emissions had been pursued by various countries in recent years. However, the energy structure was still dominated by fossil fuels, whose incomplete combustion could inevitably generate the production of pollutants such as NO<sub>x</sub>, carbon oxides, and harmful soot particles. The soot could reduce the efficiency of combustion, damage the environment, and endanger human health (Wang 2011; Dong et al. 2023). Therefore, it was important to explore technologies that could reduce dependence on

fossil fuel sources, such as renewable energy sources and carbon-free fuel combustion.

Ammonia (NH<sub>3</sub>) could be a viable clean fuel, with a 2018 report in the journal of Science lauding it as "liquid sunlight" that would provide a renewable, carbon-free energy source (Service 2018). NH<sub>3</sub> also had potential benefits and technical advantages as a sustainable fuel for power generation on vehicles. In particular, NH<sub>3</sub> was more effective than other fuels, had a longer driving range, and was more compact and cost-effective (Zamfirescu and Dincer 2009). Additionally, the octane rate of NH<sub>3</sub> was high, reaching about 110–130 (Sonker et al. 2022). The applications of NH<sub>3</sub> as fuel in gas turbines, pulverized coal co-combustion and industrial furnaces have been very successful in recent years (Kobayashi et al. 2019).

Given ammonia flame instability and low combustion intensity (Lhuillier et al. 2020; Zhou et al. 2021), researchers have been motivated to study its mixing with hydrocarbon fuels such as methane and ethylene (Chen and Liu 2023). Firstly, the combustion of the methane mixing ammonia (Grcar et al. 2004; Shu et al. 2021; Li et al. 2021) has been explored. It revealed that as the proportion of mixed NH<sub>3</sub> increased in the CH<sub>4</sub>/NH<sub>3</sub> turbulent premixed flame, the maximum flame surface density decreased, leading to

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a decrease in the ratio of the turbulent combustion velocity of  $\text{NH}_3$  to the unstretched laminar combustion velocity (Ichikawa et al. 2019). The primary way in which ammonia affected the velocity of the  $\text{CH}_4/\text{NH}_3$  flame was by altering the concentration of H and OH radicals. The sensitivity of flame to stretch increased with equivalence ratio and  $\text{NH}_3$  concentration (Okafor et al. 2018). Secondly, ethylene ( $\text{C}_2\text{H}_4$ ), as the simplest alkene, has been established its detailed combustion reaction mechanism. For microgravity ethylene diffusion flames, researchers (Lecoustre et al. 2012) have evaluated experimentally and numerically that soot formation occurred in regions where the C/O atom ratio and temperature exceeded critical values of 0.53 and 1305 K, respectively. Moreover, the local C/O atomic ratio associated with soot incipience was lower in terrestrial gravity, falling within the range of 0.32 to 0.44 (Frolov et al. 2023). The carbon atom number and C/H ratio of the final soot particles in ethylene combustion were approximately twice that of methane combustion (Wang et al. 2021). Therefore, the soot production in ethylene turbulent flames after nitrogen was replaced by hydrogen or ammonia was studied (Boyet et al. 2021). It was found that hydrogen substitution increased soot production, while ammonia addition inhibited soot formation. Additionally, the replacement of some Ar by  $\text{NH}_3$  in ethylene premixed flame was responsible for the decrease of the maximum mole fractions of  $\text{C}_4\text{H}_2$  and C5 to C10 species (Renard et al. 2009). In the  $\text{C}_2\text{H}_4$  diffusion flame, it was revealed that  $\text{NH}_3$  delayed and suppressed the formation of polycyclic aromatic hydrocarbons (PAHs), and  $\text{NH}_3$  had a greater reduction influence than Ar (Ren et al. 2022). By some kinetic studies, some researchers also found that doping ammonia decreased soot particle size, the volume fraction of soot particles and the mole fractions of soot precursors both in laminar premixed (Shao et al. 2022) and diffusion (Liu et al. 2021; Zhang et al. 2023) ammonia/ethylene flames. Then through the kinetic analyses of the mole fractions of typical soot precursors (Deng et al. 2022), it was found that  $\text{NH}_3$  addition inhibited the production of important precursor polycyclic aromatic hydrocarbons, which was mainly due to the chemical effects of  $\text{NH}_3$  in  $\text{C}_2\text{H}_4/\text{NH}_3$  diffusion flame. Furthermore, the soot from ethylene/ammonia laminar flames was experimentally and numerically studied, and found that the reduction of soot formation was mainly due to the chemical effects of  $\text{NH}_3$  (Bennett et al. 2020). However, it was not completely separate the chemical effect of  $\text{NH}_3$  from its thermal and dilution effects (Liu et al. 2015a). It could be concluded that mixing ammonia with traditional hydrocarbon fuels improved the combustion properties of ammonia and inhibit the formation of soot precursors. However, it was not clear what factors will affect the chemical effects of  $\text{NH}_3$  on  $\text{C}_2\text{H}_4$  combustion chemistry, such as different diluents.

It had been found that different diluent gas could affect the reaction kinetics and change the thermophysical properties of the mixture such as specific heats, diffusion coefficients, etc. to change the combustion temperature or reduce the generation of pollutants (Vancoillie et al. 2013; Chen et al. 2022). Researchers (Yelverton and Roberts 2008) have measured the soot surface temperature in pure and diluted ethylene co-flow diffusion flames, using helium (He), argon (Ar), nitrogen ( $\text{N}_2$ ), or carbon dioxide ( $\text{CO}_2$ ) individually. It revealed that the addition of a diluent cooled the soot surface. The He-diluted flames were the warmest and the  $\text{CO}_2$ -diluted flames were the coolest. In addition, the sensitivity of the DME flame velocity to the H-atom production and consumption reactions also decreased with the dilution of  $\text{CO}_2$ . In the lean DME flame, both the inert third-body effect and the kinetic effect of  $\text{CO}_2$  reduced the H-atom production. For the rich DME flame, the inert third-body effect increased the formation of H-atom by inhibiting the kinetic effect of  $\text{CO}_2$  (Liu et al. 2013). Focusing on the soot formation in  $\text{CO}_2$ -diluted environments, researchers performed experiments on ethylene fuel pyrolysis with varying levels of  $\text{CO}_2$  dilution and found that 25%  $\text{CO}_2$  tended to increase soot production while a higher level of  $\text{CO}_2$  reduced soot formation (Abián et al. 2012). In laminar co-flow  $\text{C}_2\text{H}_4$ /air diffusion flames, it concluded that the concentrations of the critical soot formation species, including H,  $\text{C}_2\text{H}_2$ , benzene, and pyrene were lowered in the  $\text{CO}_2$ -diluted flames due to the additional chemical effects of  $\text{CO}_2$ .  $\text{CO}_2$  remained more effective than  $\text{N}_2$  as a diluent to suppress soot formation at elevated pressures (Liu et al. 2015). The chemical effects of adding  $\text{CO}_2$  to the fuel side or oxidant side were simulated in counter-current ethylene/air diffusion flame, and it concluded that  $\text{CO}_2$  could suppress soot formation by lowering both temperature and acetylene concentration and enhancing the concentration of OH radical (Liu et al. 2001).

It may be concluded that the combustion atmosphere had very significant influences on the combustion process. However, most of the available studies have focused on the effects of diluents on the combustion of hydrocarbon fuels. The studies of the effects of diluents on ethylene/ammonia counter-flow diffusion flames were limited. Therefore, the aim of this paper was to investigate the combustion chemistry of  $\text{C}_2\text{H}_4/\text{NH}_3$  with various diluents via chemical kinetics analyses. The chemical effects of  $\text{NH}_3$  addition on the flame temperature, typical radical species, and important intermediate species were analyzed, with particular attention to the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  on the combustion process. The present study had the potential to give a better understanding of the fundamental ammonia combustion with different diluents, and to provide a reference for the detailed alteration of soot precursors and the control of other pollutant emissions.

## 2 Kinetic modeling and analysis method

The counter-flow diffusion flame simulations were performed using the CHEMKIN/OPPDIF module. The detailed chemical mechanism employed here was KM2-G, which involved 202 species and 1351 reactions (Wang et al. 2013). The KM2-G mechanism coupled a comprehensive model for nitrogen chemistry with the KM2 hydrocarbon-PAH mechanism (Zhou et al. 2022). The nitrogen chemistry included the oxidation of  $\text{NH}_3$  and the formation of nitric oxide species, which have been well validated against experimental data (Glarborg et al. 2018). The KM2 mechanism was also shown to perform excellently in terms of the prediction of the first aromatic ring as well as soot formation (Wang et al. 2020).

The separation distance between the two nozzles of the counter-flow diffusion flame burner was 8 mm. With the pressure condition of 1 atm, the inlet velocities of the fuel and oxidizer were set at 25 cm/s, and the initial temperature was 300 K. Considering that  $\text{N}_2$  was unstable at high temperatures, and could produce thermal  $\text{NO}_x$  that affected the combustion chemistry of  $\text{NH}_3$ . Therefore, as the basic working condition, the fuel side consisted of 80%  $\text{C}_2\text{H}_4 + 20\%$  Ar, and the oxidizer side was 21%  $\text{O}_2 + 79\%$  Ar. Then He and  $\text{CO}_2$  replaced the diluent gas Ar on the fuel side or the oxidizer side. Additionally, the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  were further analyzed by introducing the fictitious inert  $\text{CO}_2$  and  $\text{NH}_3$ . The specific working conditions were shown in Tables 1 and 2. In Table 1, F1–F5 represented the conditions of the  $\text{C}_2\text{H}_4/\text{NH}_3$  flames with Ar dilution and different  $\text{NH}_3$  additions. F6–F10 and F11–F15 illustrated the conditions of the

$\text{C}_2\text{H}_4/\text{NH}_3$  flames with He dilution on the fuel side and oxidizer side, respectively, and different  $\text{NH}_3$  additions. In Table 2, F1–F9 outlined the conditions of the  $\text{C}_2\text{H}_4/\text{NH}_3$  flames with  $\text{CO}_2$  dilution on the fuel side and various  $\text{NH}_3$  additions, F10–F18 delineated the conditions of the  $\text{C}_2\text{H}_4/\text{NH}_3$  flames with  $\text{CO}_2$  dilution on the oxidizer side and various  $\text{NH}_3$  additions.

As the effects of additives on fuel combustion were divided into three types: (1) dilution effects resulting from the decrease of reactive species mole fractions and collision frequencies, (2) thermal effects as a result of flame temperature variation, and (3) chemical effects caused by the participation of additives in chemical reactions (Du et al. 1990).

These three effects were highly coupled which made it quite difficult to discuss them separately. Therefore, the fictitious species method, which was firstly proposed by Liu et al. (2001) and had been employed by many researchers to analyze the specific effects of additives in different flames (as shown in Table 3), could isolate the chemical effects of additives from the dilution and thermal effects. In the study, in order to identify the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$ , normal active  $\text{CO}_2$  (denoted as  $\text{CO}_2$ ) and fictitious inert  $\text{CO}_2$  (denoted as  $\text{FCO}_2$ ) were also introduced for comparisons (Liu et al. 2003, 2015; Gu et al. 2016; Naseri et al. 2017). Similarly, the normal active  $\text{NH}_3$  was denoted as  $\text{NH}_3$ , and the fictitious inert  $\text{NH}_3$  was denoted as  $\text{FNH}_3$ . Although the fictitious species could not be directly added to real flames, in the numerical strategy,  $\text{FCO}_2$  and  $\text{CO}_2$  had the same thermodynamic parameters, transport parameters, and third-body collision efficiency, and the only difference was that  $\text{FCO}_2$  did not participate in any relevant chemical

**Table 1** Detailed flame conditions with Ar and He dilution (Unit for reactants is mole fractions)

No.	Fuel side					Oxidizer side		
	$\text{C}_2\text{H}_4$	Ar	He	$\text{NH}_3$	$\text{FNH}_3$	$\text{O}_2$	Ar	He
F1	0.8	0.2				0.21	0.79	
F2	0.6	0.2		0.2		0.21	0.79	
F3	0.6	0.2			0.2	0.21	0.79	
F4	0.4	0.2		0.4		0.21	0.79	
F5	0.4	0.2			0.4	0.21	0.79	
F6	0.8		0.2			0.21	0.79	
F7	0.6		0.2	0.2		0.21	0.79	
F8	0.6		0.2		0.2	0.21	0.79	
F9	0.4		0.2	0.4		0.21	0.79	
F10	0.4		0.2		0.4	0.21	0.79	
F11	0.8	0.2				0.21		0.79
F12	0.6	0.2		0.2		0.21		0.79
F13	0.6	0.2			0.2	0.21		0.79
F14	0.4	0.2		0.4		0.21		0.79
F15	0.4	0.2			0.4	0.21		0.79

**Table 2** Detailed flame conditions with CO<sub>2</sub> dilution (Unit for reactants is mole fractions)

No.	Fuel side						Oxidizer side			
	C <sub>2</sub> H <sub>4</sub>	Ar	CO <sub>2</sub>	FCO <sub>2</sub>	NH <sub>3</sub>	FNH <sub>3</sub>	(Oxidizer side) O <sub>2</sub>	Ar	CO <sub>2</sub>	FCO <sub>2</sub>
F1	0.8		0.2				0.21	0.79		
F2	0.6		0.2		0.2		0.21	0.79		
F3	0.6		0.2			0.2	0.21	0.79		
F4	0.6			0.2	0.2		0.21	0.79		
F5	0.6			0.2		0.2	0.21	0.79		
F6	0.4		0.2		0.4		0.21	0.79		
F7	0.4		0.2			0.4	0.21	0.79		
F8	0.4			0.2	0.4		0.21	0.79		
F9	0.4			0.2		0.4	0.21	0.79		
F10	0.8	0.2					0.21		0.79	
F11	0.6	0.2			0.2		0.21		0.79	
F12	0.6	0.2				0.2	0.21		0.79	
F13	0.6	0.2			0.2		0.21			0.79
F14	0.6	0.2				0.2	0.21			0.79
F15	0.4	0.2			0.4		0.21		0.79	
F16	0.4	0.2				0.4	0.21		0.79	
F17	0.4	0.2			0.4		0.21			0.79
F18	0.4	0.2				0.4	0.21			0.79

reactions. In this way, the dilution and thermal effects, which were similar and commonly both be classified as pure physical effects, were consistent. While the chemical effects of CO<sub>2</sub>, which not only affected the main combustion products (CO, H<sub>2</sub>) but also could play an important role in soot evolution, could be isolated (Zhao and Liu 2022). It could be considered that the variation of the flame temperatures and species concentration between the FCO<sub>2</sub> and the CO<sub>2</sub> flames was purely caused by the chemical effects. The similar method was also used for NH<sub>3</sub>. The differences between the results from NH<sub>3</sub> and FNH<sub>3</sub> additions were attributed to the NH<sub>3</sub> chemical effects, and the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> could be suggested from the differences between the CO<sub>2</sub>/NH<sub>3</sub> and FCO<sub>2</sub>/FNH<sub>3</sub> flames (Liu 2014; Li et al. 2015; Ying and Liu 2015; Liu 2015a; Luo and Liu 2017; Pan and Liu 2017; Deng et al. 2022; Zhao and Liu 2022).

## 3 Results and discussion

### 3.1 With Ar or He dilution

The effects of NH<sub>3</sub> addition on the flame temperature, major species, free radicals and important intermediate

species with Ar or He dilution were investigated, with emphasis on distinguishing the detailed effects of dilution, thermal and chemical effects of NH<sub>3</sub>.

#### 3.1.1 Flame temperature profiles

The effects of NH<sub>3</sub> with Ar or He dilution on the flame temperatures were shown in Fig. 1. The dilution and thermal effects of NH<sub>3</sub> resulted in temperature differences between 0% NH<sub>3</sub> and 20% FNH<sub>3</sub> additions, and the differences between 20% NH<sub>3</sub> and 20% FNH<sub>3</sub> additions were due to the chemical effects of NH<sub>3</sub>. The combined influences of dilution, thermal, and chemical effects led to the differences between 0% NH<sub>3</sub> and 20% NH<sub>3</sub> additions. For clarity of exposition, the specific effects were marked in Fig. 1.

In Fig. 1, the chemical effects of NH<sub>3</sub> increased the flame temperature, whereas the dilution and thermal effects of NH<sub>3</sub> caused the temperature to decrease. Consequently, the flame temperature was reduced due to the dilution and thermal effects of NH<sub>3</sub>, which had a more pronounced influence on the flame temperature than the chemical effects. The data in Fig. 1c showed that when He replaced Ar on the oxidizer side, the peak flame temperature was slightly lower, which may be due to the higher thermal diffusivity of He (Yelverton and Roberts 2008).

**Table 3** Summary of the studies using fictitious species to isolate the chemical effects

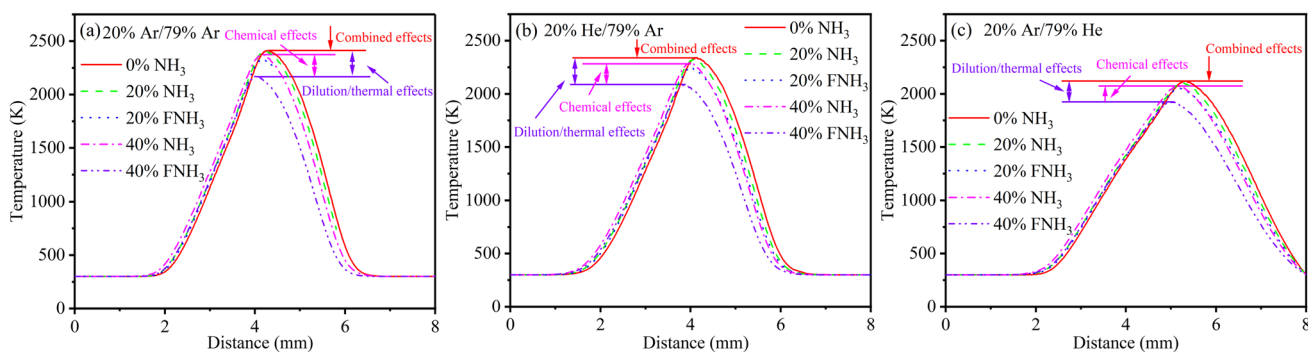
Reference	Fuel and burner types	Additives	Results
Liu et al. (2001)	Ethylene counter-flow diffusion flames	FCO <sub>2</sub>	The chemical effects of CO <sub>2</sub> addition reduced concentration of acetylene and flame temperature and conversion of carbon dioxide by hydrogen atom to hydroxyl
Park et al. (2003)	H <sub>2</sub> -O <sub>2</sub> counter-flow diffusion flames	X(CO <sub>2</sub> )	Chemical effects due to thermal dissociation of added CO <sub>2</sub> caused the reduction flame temperature in addition to some thermal effects
Guo and Smallwood (2008)	Ethylene co-flow diffusion flames	XCO <sub>2</sub>	The chemical effect of CO <sub>2</sub> addition was primarily caused by the reduced concentration of radical H, which suppressed the soot inception and surface growth rate
Liu (2014)	Premixed laminar low-pressure dimethyl ether flames	F-H <sub>2</sub> /F-O <sub>2</sub>	The chemical effects of H <sub>2</sub> addition caused the DME profile to move toward the upstream side and could suppress the production of acetylene and ethylene
Ying and Liu (2015)	Laminar premixed stoichiometric methane-air flames	F-H <sub>2</sub> /F-O <sub>2</sub>	Chemical effects of H <sub>2</sub> additive suppressed the formation of acetylene and ketene, and facilitated the productions of formaldehyde and acetaldehyde
Liu (2015b)	Premixed ethylene/ethanol flames	F-Ethanol	The ethanol chemical effects promoted formations of hazardous pollutants formaldehyde and acetaldehyde, and especially were responsible for the significant increase of acetaldehyde
Gu et al. (2016)	Axisymmetric laminar co-flow ethylene/air diffusion flames	FH <sub>2</sub> /FCO <sub>2</sub>	The chemical interactions between hydrogen and carbon dioxide on soot formation were weak
Naseri et al. (2017)	Premixed laminar ethylene/oxygen/argon burner stabilized stagnation flames	FCO <sub>2</sub>	The addition of CO <sub>2</sub> reduced the concentrations of H, C <sub>2</sub> H <sub>2</sub> , C <sub>6</sub> H <sub>6</sub> , and large PAHs which all suppressed the soot formation process through a chemical effect
Pan and Liu (2017)	Laminar lean premixed dimethyl ether flames	FH <sub>2</sub> /FCO <sub>2</sub>	The coupled effects of H <sub>2</sub> /CO <sub>2</sub> additions on major species, intermediate stable species and radicals were discussed and analyzed in detail
Mahmoud et al. (2019)	Ethylene counter-flow diffusion flames	FCO <sub>2</sub> /FH <sub>2</sub> O	The detailed chemical roles of CO <sub>2</sub> and H <sub>2</sub> O at different stages of soot formation were numerically investigated
Deng et al. (2022)	Ethylene counter-flow diffusion flames	FNH <sub>3</sub>	The flame temperature and the mole fraction profiles affected by the chemical effects of NH <sub>3</sub> addition for major species, free radicals, intermediate species, aromatics, and soot were analyzed

### 3.1.2 Major species and radicals

The mole fraction profiles of the fuel C<sub>2</sub>H<sub>4</sub> with different NH<sub>3</sub> additions were shown in Fig. 2. The differences between the NH<sub>3</sub> addition and FNH<sub>3</sub> addition revealed that the chemical effects of NH<sub>3</sub> could slightly accelerate fuel consumption. In Fig. 2c, as He replaced Ar on the oxidizer side (F11–F15 conditions in Table 1), the profiles shifted toward the oxidizer side. To analyze the detailed consumption of C<sub>2</sub>H<sub>4</sub>, the C<sub>2</sub>H<sub>4</sub> rates of production were performed in Fig. 3, it could be found that when the diluent was Ar (F1–F5 conditions in Table 1), C<sub>2</sub>H<sub>4</sub> was mainly consumed by radicals, including C<sub>2</sub>H<sub>4</sub> + H = C<sub>2</sub>H<sub>3</sub> + H<sub>2</sub> and C<sub>2</sub>H<sub>4</sub> + OH = C<sub>2</sub>H<sub>3</sub> + H<sub>2</sub>O reactions. The rates of these reactions responsible for the

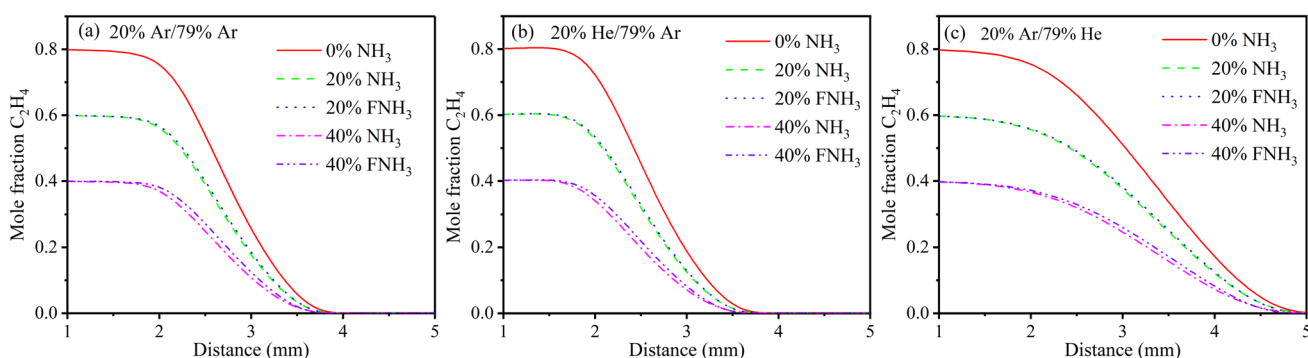
depletion of C<sub>2</sub>H<sub>4</sub> decreased with the addition of NH<sub>3</sub>, which dominated the chemical effects. Therefore, it was necessary to analyze the mole fractions of these typical radicals, including H, O, and OH radicals.

Figure 4 gave the mole fractions of the H radical with different NH<sub>3</sub> additions. When the dilution gas was Ar (F1–F5 conditions in Table 1) or He (F6–F15 conditions in Table 1), the mole fractions of H radical decreased with increasing concentrations of NH<sub>3</sub> additive, and with 20% NH<sub>3</sub> addition, the chemical effects of NH<sub>3</sub> further reduced H concentration. While the blending ratio was 40%, the chemical effects of NH<sub>3</sub> increased the mole fraction of H radical when the dilution gas was only Ar (as shown in Fig. 4a). The results were consistent with Deng et al. (2022) and Zhang et al. (2023).

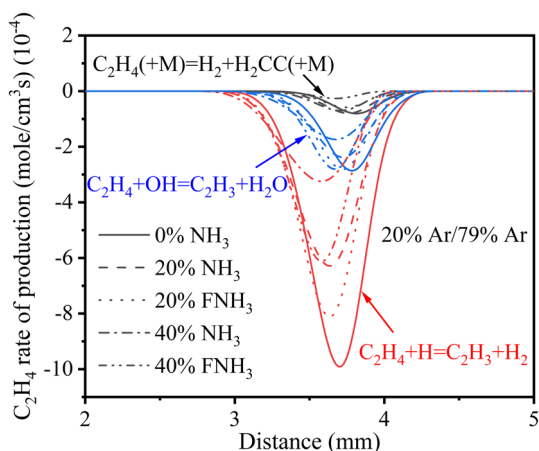


**Fig. 1** Flame temperature with Ar or He dilution and different NH<sub>3</sub> additions. *Notes:* The 20% Ar/79% Ar represented the dilution gas was Ar both on the fuel side and the oxidizer side (F1-F5 conditions in Table 1). The 20% He/79% Ar and the 20% Ar/79% He represented

dilution gas He replaced Ar on the fuel side (F6-F10 conditions in Table 1) and the oxidizer side (F11-F15 conditions in Table 1). The annotations for Figs. 2, 3, 4, 5, 6, 7, 8 and 9 have the same meanings, which will not be noted again in the following



**Fig. 2** Mole fraction profiles of C<sub>2</sub>H<sub>4</sub> with Ar or He dilution and different NH<sub>3</sub> additions

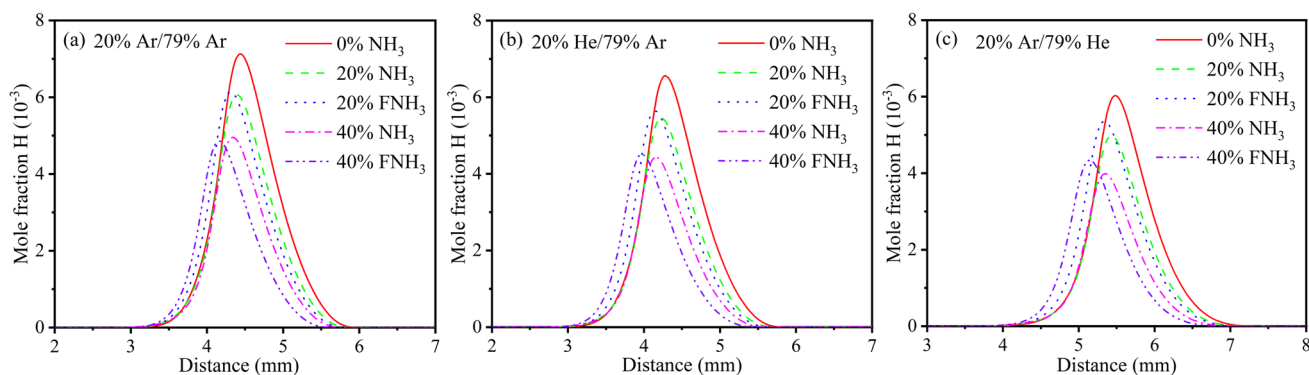


**Fig. 3** Rate of production of C<sub>2</sub>H<sub>4</sub> with different NH<sub>3</sub> additions

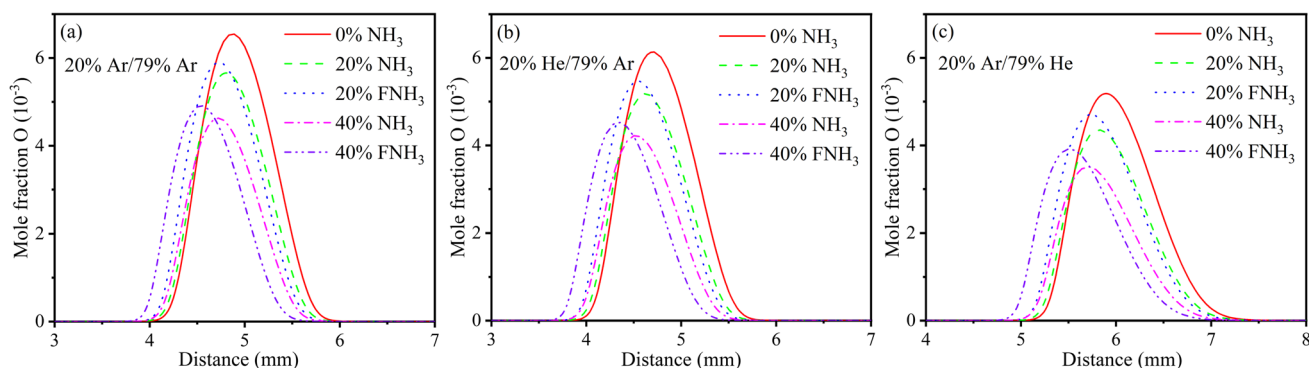
Oxidation of PAH and soot particles may occur subsequent to formation in diffusion flames and the main oxidation reactants were OH, O, and O<sub>2</sub> (Richter and Howard

2000). Therefore, it was necessary to analyze the mole fraction profiles of the O radical, which were shown in Fig. 5. Comparing the O radical mole fractions with NH<sub>3</sub> and FNH<sub>3</sub> additions, it illustrated that the chemical effects of NH<sub>3</sub> could inhibit the formation of O radical regardless of the different dilution gas.

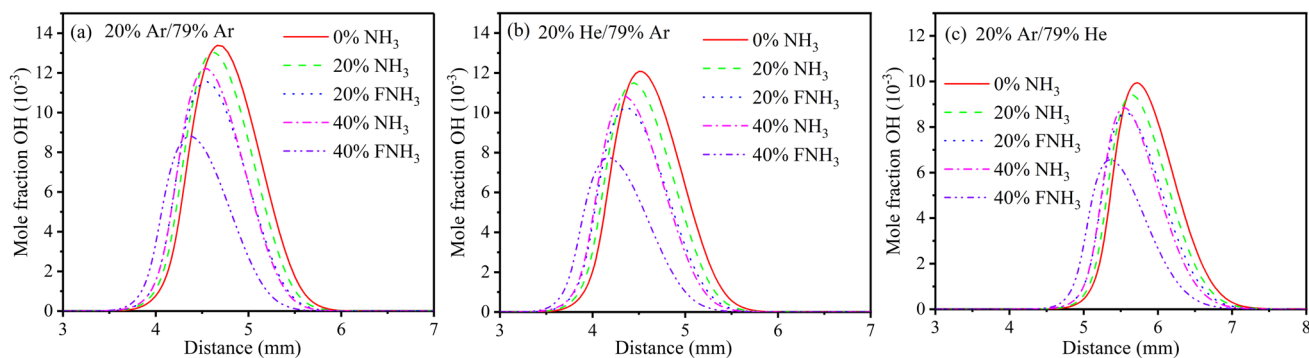
Furthermore, hydroxyl OH played a dominant role in the soot generation area of counter-flow diffusion flame, due to the relatively low concentration of O<sub>2</sub>. The OH radical was mainly oxidized by reacting with the active sites on the surface of soot, which could inhibit the further generation of soot (Frenklach et al. 2018). The mole fraction profiles were performed in Fig. 6. The addition of NH<sub>3</sub> also suppressed the formation of OH radical, but different from the effects on O, H radicals, it was primarily because of the dilution and thermal effects of NH<sub>3</sub>, which were more pronounced than its chemical effects. Notably, the mole distributions of OH radical with NH<sub>3</sub> addition were higher than those with FNH<sub>3</sub> addition, indicating that the chemical effect of NH<sub>3</sub> promoted the formation of OH radical indeed.



**Fig. 4** Mole fraction profiles of H with Ar or He dilution and different  $\text{NH}_3$  additions



**Fig. 5** Mole fraction profiles of O with Ar or He dilution and different  $\text{NH}_3$  additions

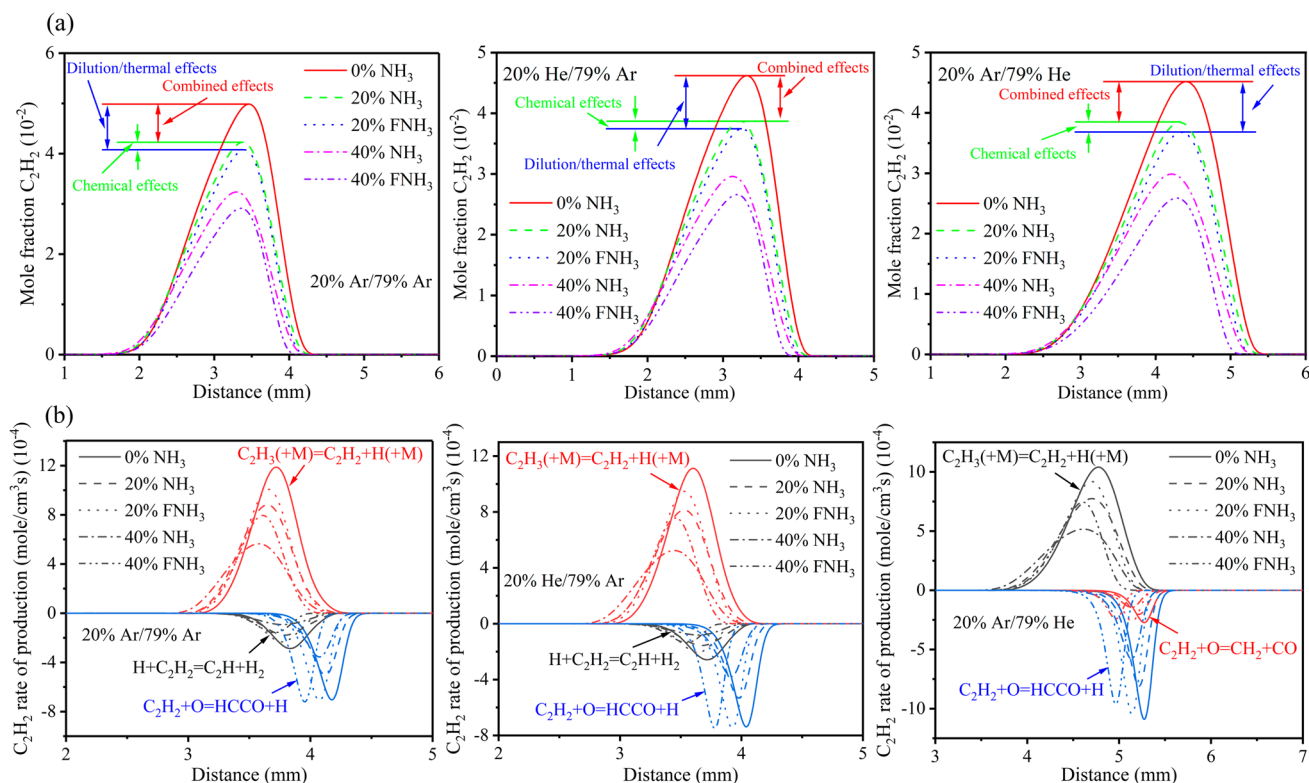


**Fig. 6** Mole fraction profiles of OH with Ar or He dilution and different  $\text{NH}_3$  additions

### 3.1.3 Intermediate hydrocarbon species

The intermediate hydrocarbon species would be oxidized with radicals to inhibit the soot formation to some extent. Therefore, the mole fractions of acetylene ( $\text{C}_2\text{H}_2$ ), propynyl ( $\text{C}_3\text{H}_3$ ), and benzene (A1), which were important soot precursors, in the combustion process of  $\text{C}_2\text{H}_4/\text{NH}_3$  diluted with Ar (F1–F5 conditions in Table 1) or He (F6–F15 conditions

in Table 1) were shown in Figs. 7, 8 and 9. It could be found that the combined effects of the  $\text{NH}_3$  additive reduced the mole fractions of these important intermediate hydrocarbon species from Figs. 7a, 8a and 9a. The similar results had been achieved by Li et al. (2021), Shao et al. (2022) and Ren et al. (2022). In Fig. 7a, the differences between the mole distributions of  $\text{C}_2\text{H}_2$  with  $\text{NH}_3$  addition and  $\text{FNH}_3$  addition demonstrated that the chemical effects of  $\text{NH}_3$  promoted the



**Fig. 7** Mole fractions and Rates of production of  $C_2H_2$  with Ar or He dilution and different  $NH_3$  additions. **a** Mole fractions; **b** Rates of production

formation of  $C_2H_2$ . Similarly, the chemical effects of  $NH_3$  were also observed to increase the mole fractions of  $C_3H_3$  and A1, as shown in subsequent Figs. 8a and 9a. Therefore, regardless of the dilution environment, the productions of  $C_2H_2$ ,  $C_3H_3$ , and A1 were inhibited due to the dilution and thermal effects of  $NH_3$ , instead of the chemical effects of  $NH_3$ . It was worth pointing out that, as shown in Figs. 8a and 9a, the mole fractions of  $C_3H_3$  and A1 were much lower when He replaced Ar on the fuel side or oxidizer side (F6–F15 conditions in Table 1). It revealed that the pathway of A1 generated by small molecule  $C_3H_3$  in the  $C_2H_4/NH_3$  counter-flow diffusion flame was more easily susceptible to He.

To analyze the detailed formation and consumption of these important intermediate hydrocarbon species, the rates of production were analyzed in Figs. 7b, 8b and 9b. It could be found that the main reaction concerning  $C_2H_2$  formation was  $C_2H_3(+M) = C_2H_2 + H(+M)$ , although the dilution environment was different, and the reaction rates were greatly reduced with the chemical effects of  $NH_3$ , as shown in Fig. 7b. Whereas the rate of the main reaction  $C_2H_2 + CH_2 = C_3H_3 + H$  for  $C_3H_3$  formation was reduced mainly due to the dilution and thermal effects of  $NH_3$ , as shown in Fig. 8b. Figure 9b illustrated that the reaction  $A1 + C_2H_4 = A1 + C_2H_3$  was mainly

responsible for A1 formation, and the oxidation reaction  $A1 + H(+M) = A1(+M)$  was added when He diluted on the fuel side. Comparing the  $NH_3$  and  $FNH_3$  additions, it could be found that the chemical effects of  $NH_3$  promoted the reaction  $A1 + C_2H_4 = A1 + C_2H_3$ , whereas it suppressed other reactions.

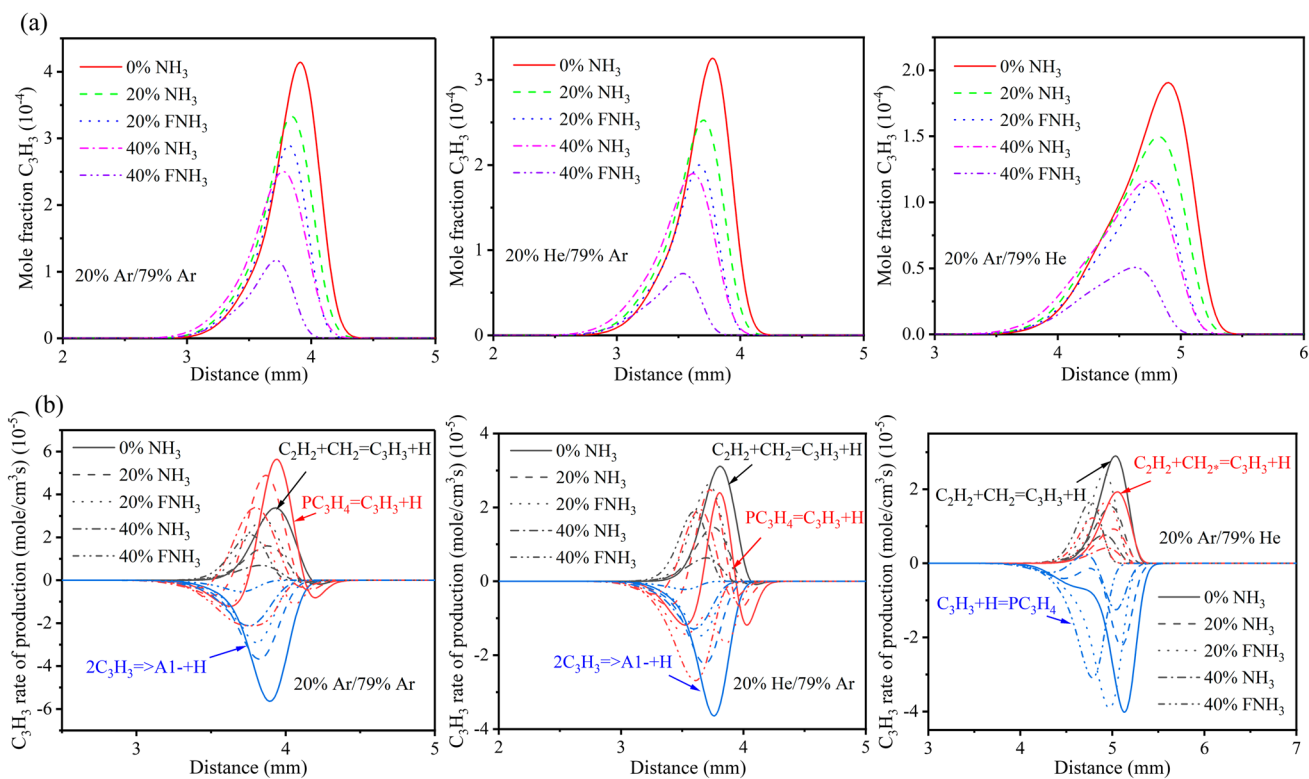
### 3.2 With $CO_2$ dilution

When  $CO_2$  was used as the diluent, the chemical effects of  $NH_3$  may be influenced by the chemical effects of  $CO_2$ . Therefore, this section would put a special emphasis on the analysis of the coupled chemical effects of  $NH_3$  and  $CO_2$  on flame temperature, major species, free radicals, important intermediate hydrocarbon species, and oxygenated species.

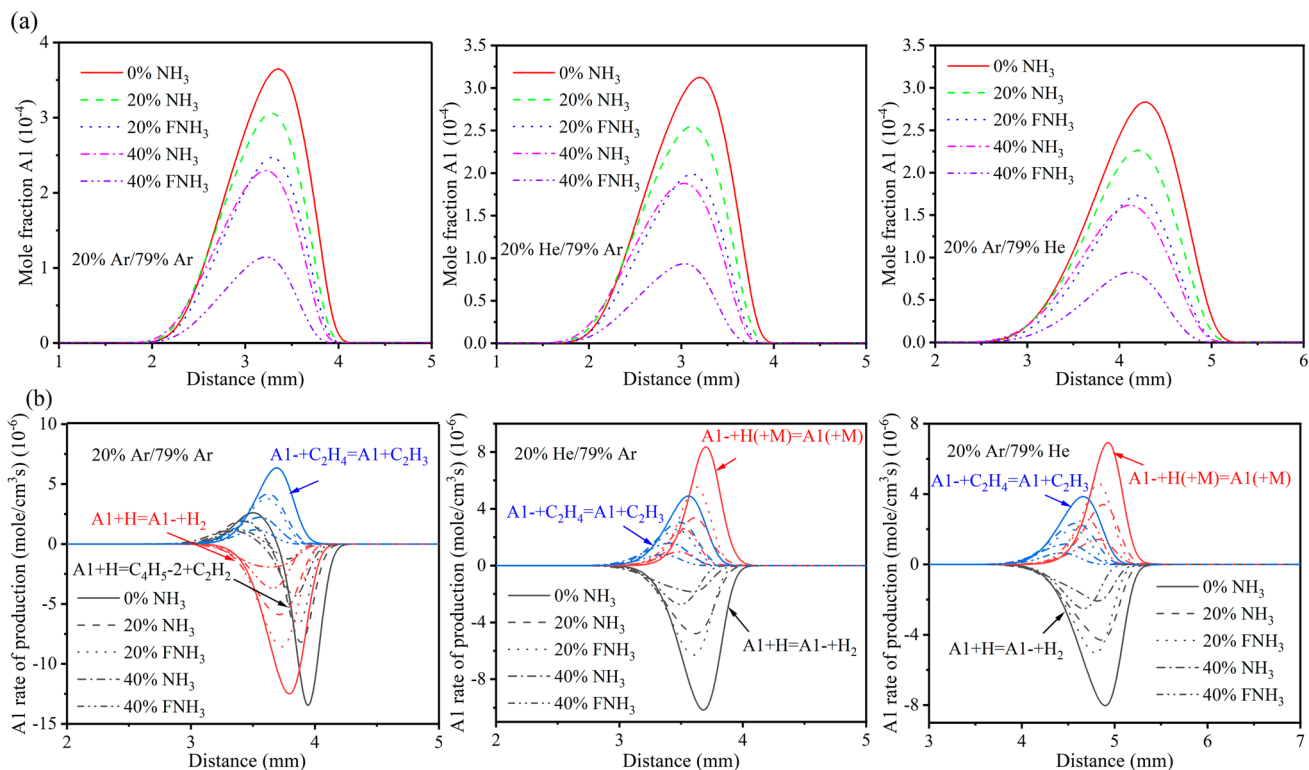
#### 3.2.1 Flame temperature profiles

As shown in Fig. 10, the addition of  $NH_3$  reduced the flame temperature. In Fig. 10a, the differences between  $CO_2/NH_3$  and  $CO_2/FNH_3$  revealed that the chemical effects of  $NH_3$  increased the temperature. The differences between  $CO_2/NH_3$  and  $FCO_2/FNH_3$  additions suggested that the coupled chemical effects of  $NH_3$  and  $CO_2$  also led to an increase in the flame temperature. However, with





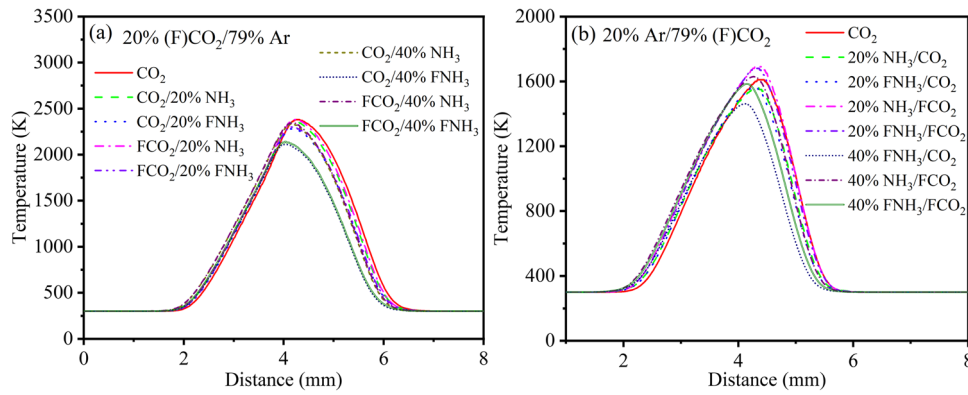
**Fig. 8** Mole fractions and Rates of production of  $C_3H_3$  with Ar or He dilution and different  $NH_3$  additions. **a** Mole fractions; **b** Rates of production



**Fig. 9** Mole fractions and Rates of production of A1 with Ar or He dilution and different  $NH_3$  additions. **a** Mole fractions; **b** Rates of production

CO<sub>2</sub> addition on the oxidizer side, as shown in Fig. 10b, the coupled chemical effects decreased the temperature. This was possibly because the chemical effects of CO<sub>2</sub> lowered the temperature (Liu et al. 2001) and were dominant with oxidizer-side addition. Meanwhile, it was worth noting that the temperature was greatly lower with the

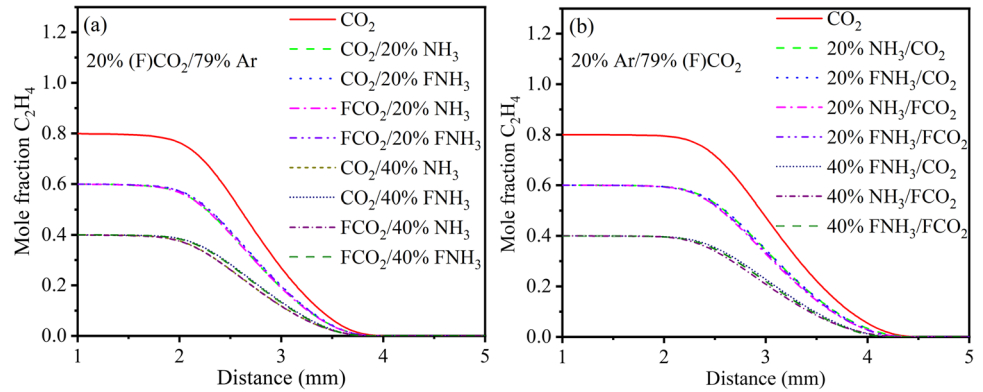
oxidizer-side CO<sub>2</sub> addition. Even when the condition was 40% NH<sub>3</sub>/79% CO<sub>2</sub> (F15 condition in Table 2), the fuel could not be ignited. Therefore, the working condition would not be discussed in the following. As the known literature data showed that the threshold local temperature for the onset of soot formation in diffusion flames,  $T_c$ ,



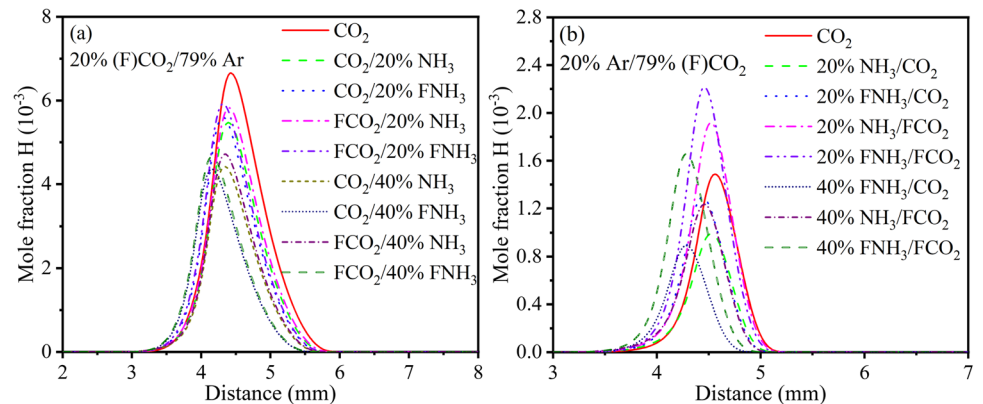
**Fig. 10** Flame temperature with CO<sub>2</sub> dilution and different NH<sub>3</sub> additions. *Notes:* The 20% (F)CO<sub>2</sub>/79% Ar and the 20% Ar/79% (F)CO<sub>2</sub> respectively represented dilution gas CO<sub>2</sub> replaced Ar on the fuel side (F1-F9 conditions in Table 2) and the oxidizer side (F10-F18 con-

ditions in Table 2). The (F)CO<sub>2</sub> represented the normal CO<sub>2</sub> (CO<sub>2</sub>) or fiction CO<sub>2</sub> (FCO<sub>2</sub>) addition. The annotations for Figs. 11, 12, 13, 14, 15, 16 and 18 have the same meanings, which will not be noted again in the following

**Fig. 11** Mole fraction profiles of C<sub>2</sub>H<sub>4</sub> with CO<sub>2</sub> dilution and different NH<sub>3</sub> additions



**Fig. 12** Mole fraction profiles of H with CO<sub>2</sub> dilution and different NH<sub>3</sub> additions



satisfied the condition  $T_c > 1300\text{--}1500\text{ K}$  (Frolov et al. 2023), the analysis of soot precursors concentrations in flame conditions were necessary.

### 3.2.2 Major species and radicals

Figure 11 gave the mole fraction profiles of  $C_2H_4$ . The comparison with the addition of 40%  $NH_3$  and 40%  $FNH_3$  illustrated that the chemical effects of  $NH_3$  reduced the  $C_2H_4$  mole fraction slightly. However, the coupled effects of  $NH_3$  and  $CO_2$  on  $C_2H_4$  were less pronounced when  $CO_2$  is added to either the fuel side or the oxidizer side.

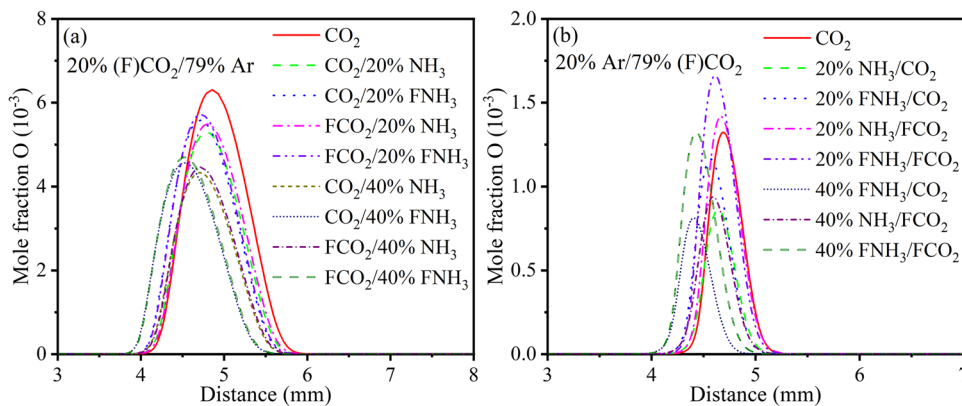
The mole fraction profiles of H radical were displayed in Fig. 12. It illustrated that the addition of  $NH_3$  decreased the H concentration. The fuel-side  $CO_2$  dilution (F1–F9 conditions in Table 2) was similar to the condition of Ar-diluted, the chemical effects of  $NH_3$  reduced H concentration with 20%  $NH_3$  addition, while increased the mole fraction of H when the blending ratio was 40%, as shown in Fig. 12a. Whereas, Fig. 12b illustrated that the chemical effects of  $NH_3$  inhibit H formation with oxidizer-side  $CO_2$  dilution (F10–F18 conditions in Table 2). The differences between the H radical of 20%  $CO_2/NH_3$  and 20%  $FCO_2/NH_3$  were owing to the chemical effects of  $CO_2$ , which could decrease the mole fraction of H radical. This was the same result as

the known literature (Liu 2015a). Moreover, the differences between  $NH_3/CO_2$  and  $FNH_3/FCO_2$  additions revealed that the reductions in H concentration were due to the coupled chemical effects of  $NH_3$  and  $CO_2$ , especially with the oxidizer-side  $CO_2$  addition. The existing literature (Liu et al. 2001; Mahmoud et al. 2019) indicated that in ethylene counter-flow diffusion flames, the flame sheet front was situated on the oxidizer side of the stagnation plane. Consequently, the addition of oxidizer may result in a more pronounced increase in the  $CO_2$  concentrations at the flame sheet. The promotion of the  $CO_2 + H = CO + OH$  reaction was also more significant for the oxidizer side addition.

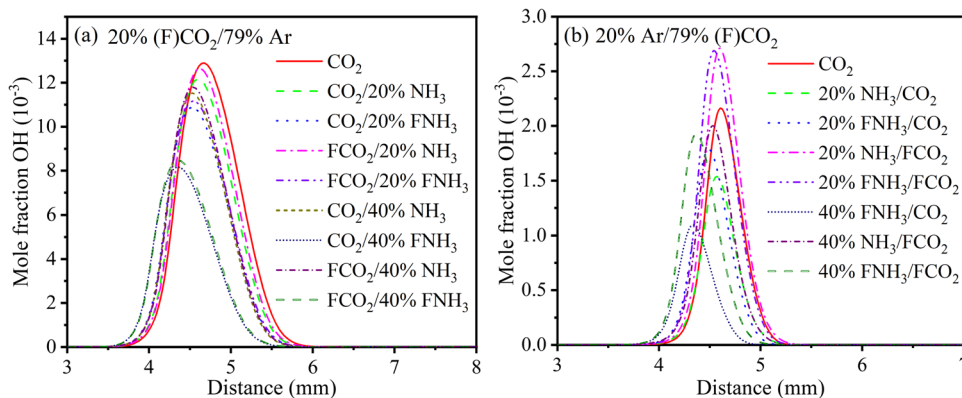
Figure 13 illustrated the mole fraction profiles of O radical. Similar to the reduction of the mole fractions of H radical, the coupled chemical effects of  $NH_3$  and  $CO_2$  reduced O radical concentration, especially with the addition of  $CO_2$  on the oxidizing side.

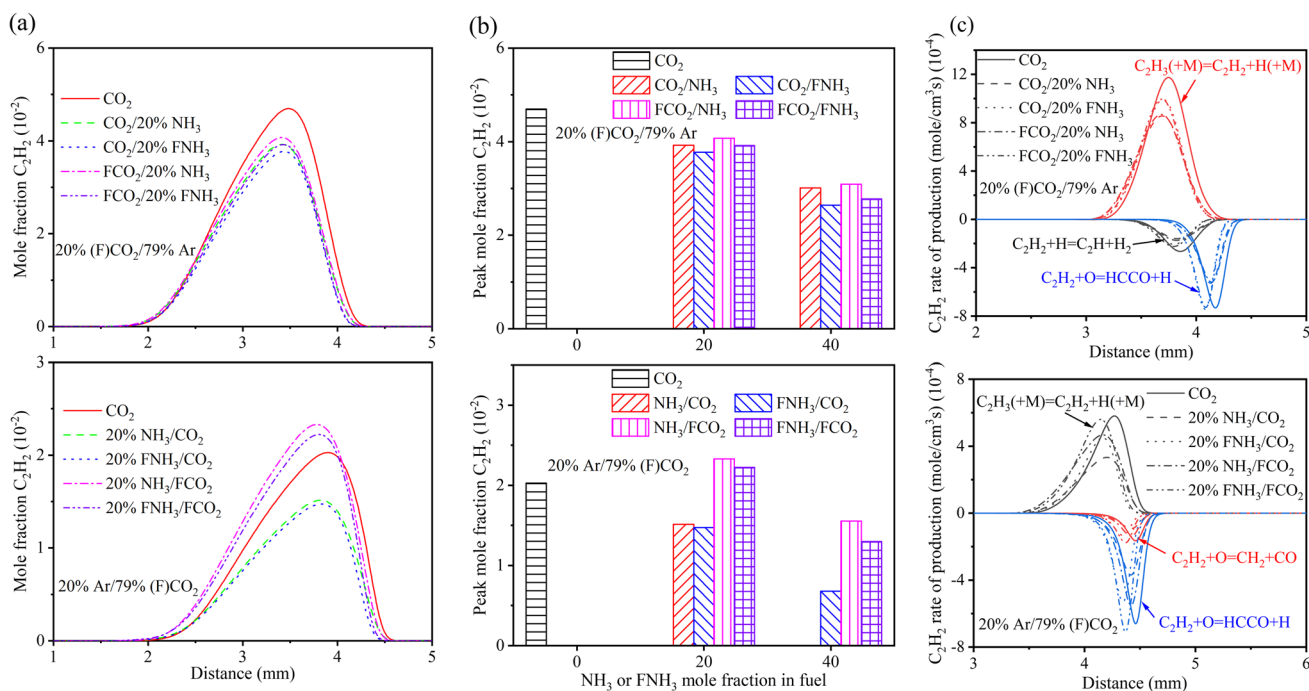
However, the coupled chemical effects of  $NH_3$  and  $CO_2$  on the mole fraction of OH radical were different. As shown in Fig. 14a, the differences between  $NH_3/CO_2$  and  $FNH_3/FCO_2$  additions revealed that the coupled chemical effects of  $NH_3$  and  $CO_2$  promoted the formation of OH with fuel-side  $CO_2$  addition. Nevertheless, the coupled chemical effects had obvious inhibitory effects when  $CO_2$  addition on the oxidizer side, which were shown in Fig. 14b. It was possibly

**Fig. 13** Mole fraction profiles of O with  $CO_2$  dilution and different  $NH_3$  additions



**Fig. 14** Mole fraction profiles of OH with  $CO_2$  dilution and different  $NH_3$  additions





**Fig. 15** Mole fractions and Rates of production of  $C_2H_2$  with  $CO_2$  dilution and different  $NH_3$  additions. **a** Mole fractions; **b** Peak mole fractions; **c** Rates of production

because the chemical effects of  $CO_2$  also decreased the OH radical mole fractions, which could be found from the differences between  $NH_3/CO_2$  and  $NH_3/FCO_2$  additions. And with the oxidizer-side  $CO_2$  dilution, the chemical effects of  $CO_2$  were more significant.

### 3.2.3 Intermediate hydrocarbon species

$C_2H_2$  was considered to be an important small molecule precursor of soot formation (Ruiz et al. 2007; Chernov et al.

2014; Wang and Chung 2019).  $C_3H_3$  and A1 also were very vital for the soot production.

Firstly, the chemical effects of  $CO_2$  and  $NH_3$  on  $C_2H_2$  concentration were identified in Fig. 15. The differences between  $CO_2/NH_3$  and  $FCO_2/FNH_3$  additions represented the coupled chemical effects of  $NH_3$  and  $CO_2$ . Compared with Fig. 15a, b, it could be found that the coupled chemical effects of  $NH_3$  and  $CO_2$  were weak when  $CO_2$  was from the fuel side (F1–F9 conditions in Table 2), while it led to a significant reduction in the mole fractions of  $C_2H_2$  with

**Table 4** The calculation of the chemical effects of  $NH_3$  and  $CO_2$  on the peak mole fraction of  $C_2H_2$ .  $A_i$  ( $i=1, 2, 3$ ) represented the chemical effects of  $NH_3$ ,  $B_i$  ( $i=1, 2, 3$ ) represented the chemical effects of  $CO_2$ ,  $A_i + B_i$  ( $i=1, 2, 3$ ) represented the sum of the separate chemical effects of  $NH_3$  and  $CO_2$ ,  $C_i$  ( $i=1, 2, 3$ ) represented the coupled chemical effects of  $NH_3$  and  $CO_2$

Case	(F) $CO_2$ (%)	(F) $NH_3$ (%)	Conditions	The difference of the peak mole fraction $C_2H_2$ (ppm)
A1	20	20	$CO_2/NH_3$ - $CO_2/FNH_3$	1522.6
B1	20	20	$CO_2/NH_3$ - $FCO_2/NH_3$	-1469.8
A1 + B1	20	20		52.8
C1	20	20	$CO_2/NH_3$ - $FCO_2/FNH_3$	35.7
A2	20	40	$CO_2/NH_3$ - $CO_2/FNH_3$	3682.7
B2	20	40	$CO_2/NH_3$ - $FCO_2/NH_3$	-834.9
A2 + B2	20	40		2847.8
C2	20	40	$CO_2/NH_3$ - $FCO_2/FNH_3$	2343.3
A3	79	20	$NH_3/CO_2$ - $FNH_3/CO_2$	395.8
B3	79	20	$NH_3/CO_2$ - $NH_3/FCO_2$	-8167.0
A3 + B3	79	20		-7771.2
C3	79	20	$NH_3/CO_2$ - $FNH_3/FCO_2$	-7095.6

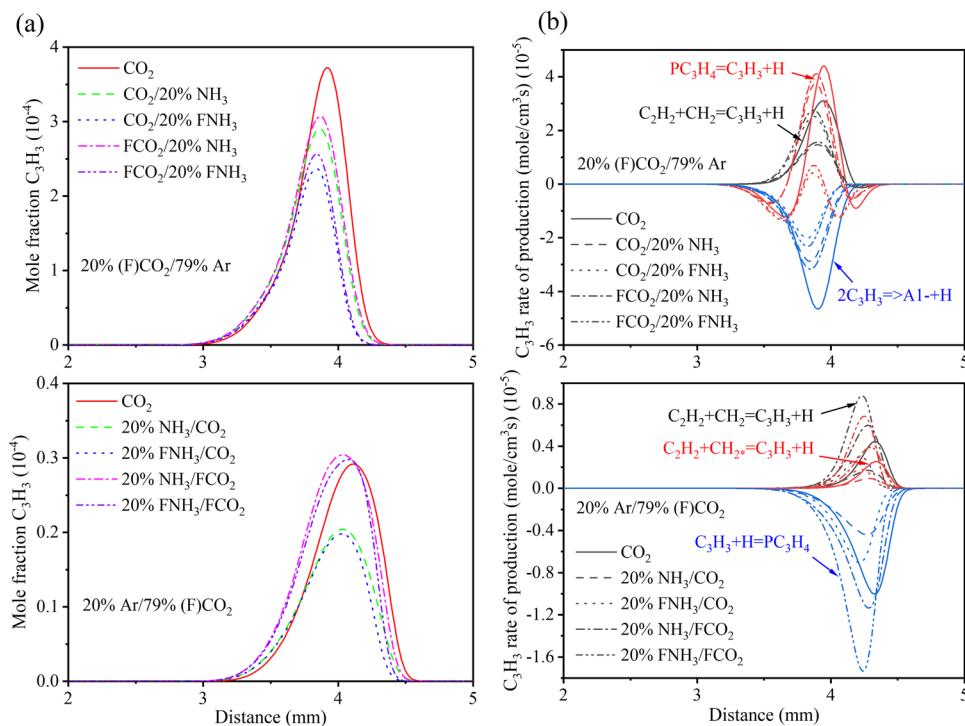
CO<sub>2</sub> addition on the oxidizer side (F10–F18 conditions in Table 2). To discover C<sub>2</sub>H<sub>2</sub> variation trends with increasing NH<sub>3</sub> additions, Fig. 15b gave the C<sub>2</sub>H<sub>2</sub> peak mole fractions. It revealed explicitly that the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> increased the mole fractions of C<sub>2</sub>H<sub>2</sub> more significantly with the concentration of NH<sub>3</sub> increasing, when CO<sub>2</sub> was added to the fuel side. Fig. 15c illustrated the rates of production analysis of C<sub>2</sub>H<sub>2</sub>, it could be found that the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> decreased the rate of the reaction C<sub>2</sub>H<sub>3</sub>(+M)=C<sub>2</sub>H<sub>2</sub>+H(+M), which was the main reaction for C<sub>2</sub>H<sub>2</sub> formation. Therefore, the participation of C<sub>2</sub>H<sub>2</sub> in the growth reaction of polycyclic aromatic hydrocarbons (PAHs) through the HACA mechanism would be affected (Frenklach 2002), then the surface growth of soot could be inhibited to some extent.

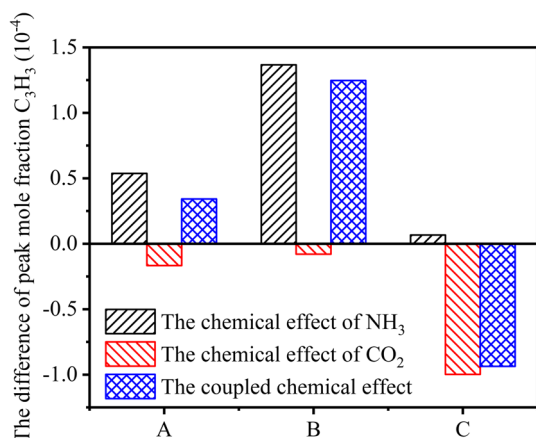
According to the peak mole fractions of C<sub>2</sub>H<sub>2</sub> shown in Fig. 15b and the calculation method shown in Table 4, the chemical effects of NH<sub>3</sub> and CO<sub>2</sub> could be demonstrated quantitatively (Pan and Liu 2017). In Table 4, Ai (*i* = 1, 2, 3) represented the chemical effects of NH<sub>3</sub> in the combined effects of NH<sub>3</sub> and CO<sub>2</sub>. Similarly, Bi (*i* = 1, 2, 3) denoted the chemical effects of CO<sub>2</sub>, Ai + Bi (*i* = 1, 2, 3) represented the sum of the separate chemical effects of NH<sub>3</sub> and CO<sub>2</sub>, Ci (*i* = 1, 2, 3) was equal to the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub>. In the results of the calculation, a positive value indicated an increase and a negative value represented a decrease. When the condition was 40% NH<sub>3</sub>/79% CO<sub>2</sub> (F15 condition in Table 2), the fuel could not be ignited, so only the coupled chemical effects of adding 20% NH<sub>3</sub>

were considered with CO<sub>2</sub> addition on the oxidizer side. The B1, B2, B3 revealed that the chemical effects of CO<sub>2</sub> suppressed the formation of C<sub>2</sub>H<sub>2</sub>, which was consistent with the known literature (Liu et al. 2001; Liu 2015a), whereas the chemical effects of NH<sub>3</sub> increased the mole fractions of C<sub>2</sub>H<sub>2</sub>. The former dominated the latter and the net effects were to reduce the mole fractions of C<sub>2</sub>H<sub>2</sub> with the oxidizer-side CO<sub>2</sub> addition, different from CO<sub>2</sub> addition on the fuel side. Compared with the (Ai + Bi) and Ci, it could be found that the changes of C<sub>2</sub>H<sub>2</sub> mole fractions in the simultaneous presence of chemical effects of NH<sub>3</sub> and CO<sub>2</sub> were slightly smaller than the sum of the separate chemical effects of NH<sub>3</sub> and CO<sub>2</sub>. It suggested that chemical interactions between the dopants were negligible, as the results of Mahmoud et al. (2019).

Figure 16 illustrated the mole fraction profiles and the rates of production of C<sub>3</sub>H<sub>3</sub>. From Fig. 16a, it could be concluded that the addition of NH<sub>3</sub> reduced the mole fractions of C<sub>3</sub>H<sub>3</sub>. The differences between NH<sub>3</sub>/CO<sub>2</sub> and FNH<sub>3</sub>/FCO<sub>2</sub> revealed that the coupled chemical effects of NH<sub>3</sub> and CO<sub>2</sub> increased the concentration of C<sub>3</sub>H<sub>3</sub> with CO<sub>2</sub> addition on the fuel side (F1–F9 conditions in Table 2), contrary to the results of the oxidizer-side CO<sub>2</sub> addition (F10–F18 conditions in Table 2). Figure 16b illustrated that C<sub>3</sub>H<sub>3</sub> was generated in large quantities by the complex reactions of C<sub>2</sub>H<sub>2</sub>+CH<sub>2</sub>, which was one of the reasons why C<sub>3</sub>H<sub>3</sub> was considered as the main precursor of A1 generated by small molecules (Jin et al. 2015), then PAHs were easy to form soot after physical or chemical coalesce. When

**Fig. 16** Mole fractions and Rates of production of C<sub>3</sub>H<sub>3</sub> with CO<sub>2</sub> dilution and different NH<sub>3</sub> additions. **a** Mole fractions; **b** Rates of production





**Fig. 17** The Difference of peak mole fractions of  $C_3H_3$ . *Notes:* A represented the fuel side was 60%  $C_2H_4$ +20%  $CO_2$ +20%  $NH_3$ , the oxidizer side was 79% Ar+21%  $O_2$ ; B represented the fuel side was 40%  $C_2H_4$ +20%  $CO_2$ +40%  $NH_3$ , the oxidizer side was 79% Ar+21%  $O_2$ ; C represented the fuel side was 60%  $C_2H_4$ +20% Ar+20%  $NH_3$ , the oxidizer side was 79%  $CO_2$ +21%  $O_2$ . The positive results represented an increase and the negative results represented a decrease. The letters in Figs. 19 and 20 have the same meanings, which will not be noted again in the following.

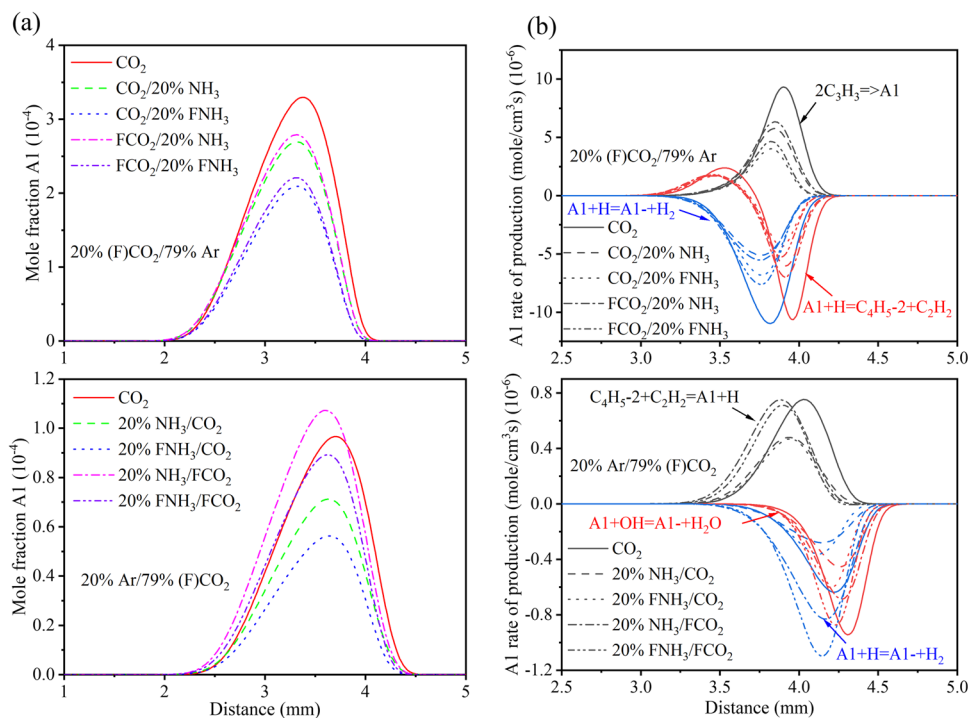
$CO_2$  was added to the oxidizer side, the coupled chemical effects of  $NH_3$  and  $CO_2$  decreased the rates of all reactions, whereas  $CO_2$  was from the fuel side, the rates of reactions  $PC_3H_4=C_3H_3+H$  and  $2C_3H_3\Rightarrow A1+H$  were decreased mainly due to the coupled dilution and thermal effects of  $NH_3$  and  $CO_2$ . The bar plot of the chemical effects of  $NH_3$  and  $CO_2$  on the peak mole fractions of  $C_3H_3$  was shown

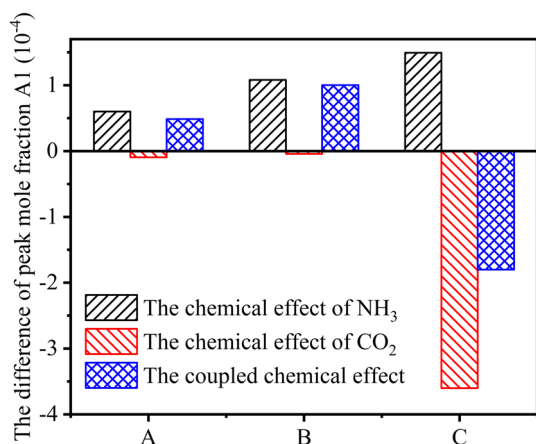
in Fig. 17. The formation of  $C_3H_3$  was inhibited mainly because of the chemical effects of  $CO_2$ , Zhang et al. (2018) also gave the similar results, while the chemical effects of  $NH_3$  promoted the formation of  $C_3H_3$ . When  $CO_2$  was added to the oxidizer side, the coupled chemical effects of  $NH_3$  and  $CO_2$  could inhibit the generation of  $C_3H_3$  due to the dominance of the chemical effects of  $CO_2$ , different from the fuel-side  $CO_2$  addition.

It was generally agreed that PAHs were the precursors of soot formation, and the unique chemical structure of benzene ring (A1) was a prominent factor (Dobbins 2007). Therefore, it was necessary to analyze the variations of A1 concentration. The mole fraction profiles of A1 performed in Fig. 18a revealed that the normal  $NH_3$  addition could cause the decrease of A1 mole fractions. However, the coupled chemical effects of  $NH_3$  and  $CO_2$  on the mole fraction of A1 were different due to the diverse sides and concentrations of  $CO_2$  addition. With the fuel-side  $CO_2$  addition (F1–F9 conditions in Table 2), the differences between  $CO_2/NH_3$  and  $FCO_2/FNH_3$  additions suggested that the coupled chemical effects of  $NH_3$  and  $CO_2$  increased the A1 mole fractions, in contradiction with adding  $CO_2$  to the oxidizer side. Meanwhile, comparing the two situations, it could be found that the concentration of A1 was much lower when  $CO_2$  was added to the oxidizer side (F10–F18 conditions in Table 2).

To analyze the detailed formation and consumption of A1, Fig. 18b gave the rates of production of A1. It could be found that the main reactions responsible for A1 formation were the closed-loop reactions  $2C_3H_3\Rightarrow A1$  and  $C_2H_2+C_4H_5-2=A1+H$ . The main reactions

**Fig. 18** Mole fractions and Rates of production of A1 with  $CO_2$  dilution and different  $NH_3$  additions. **a** Mole fractions; **b** Rates of production





**Fig. 19** The Difference of peak mole fractions of A1

responsible for A1 consumption were  $A1 + H = A1 + H_2$ ,  $A1 + H = C_4H_5 - 2 + C_2H_2$ , and  $A1 + OH = A1 + H_2O$ . The pyrolysis consumption paths were mainly through hydrogen extraction reaction attacked by H radical (Yang et al. 2015). Comparing with  $CO_2/NH_3$  and  $FCO_2/FNH_3$  additions, it could be concluded that the reduced rates of all reactions were due to the coupled chemical effects of  $NH_3$  and  $CO_2$  with the oxidizer-side  $CO_2$  addition. While adding  $CO_2$  to the fuel side, the rate of reactions  $2C_3H_3 \Rightarrow A1$  and  $A1 + H = C_4H_5 - 2 + C_2H_2$  were decreased mainly because of the coupled dilution and thermal effects of  $NH_3$  and  $CO_2$ .

By distinguishing the chemical effects of  $NH_3$  and  $CO_2$ , as shown in Fig. 19, it could be found that the chemical effects of  $NH_3$  promoted the generation of A1, while the chemical effects of  $CO_2$  suppressed it. The results tied well with previous study (Naseri et al. 2017). Therefore, the coupled chemical effects of  $NH_3$  and  $CO_2$  on A1 mole fractions depended on the dominant effects. With the oxidizer-side  $CO_2$  addition, the chemical effects of  $CO_2$  dominated the chemical effects of  $NH_3$ , then the coupled chemical effects of  $NH_3$  and  $CO_2$  decreased the mole fraction of A1. For

fuel-side  $CO_2$  addition, the chemical effects of  $NH_3$  on the A1 mole fraction were more significant and then the coupled chemical effects of  $NH_3$  and  $CO_2$  increased A1 concentration.

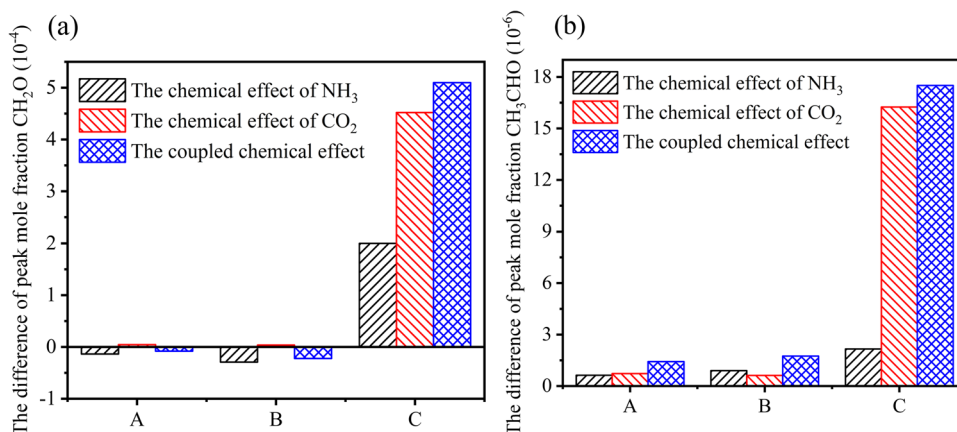
As the known literature (Liu et al. 2015), the chemical effect of  $CO_2$  on soot loading reduction was primarily through reducing the rates of soot formation steps, rather than prompting soot oxidation. Therefore, with the addition of  $CO_2$  on the oxidizer side, the coupled chemical effects of  $NH_3$  and  $CO_2$ , which were mainly influenced by the chemical effect of  $CO_2$ , reduced both the mole fractions of O, H, OH radicals, and  $C_2H_2$ ,  $C_3H_3$ , A1 soot precursors.

### 3.2.4 Intermediate oxygenated species

In addition to intermediate hydrocarbon species, intermediate oxygenated species such as formaldehyde ( $CH_2O$ ) and acetaldehyde ( $CH_3CHO$ ) were also important aldehyde contaminants generated in the combustion of hydrocarbon fuels. Formaldehyde was particularly irritant to the respiratory system and eyes, toxic and carcinogenic and could accelerate the production of the harmful substance ozone (Konnov et al. 2021). Therefore, the mole fraction profiles of  $CH_2O$  and  $CH_3CHO$  in  $C_2H_4/NH_3$  flames with diluents were necessary to be revealed in Fig. 20.

Due to the chemical effects of  $CO_2$ , the chemical effects of  $NH_3$  performed diverse impacts on  $CH_2O$  and  $CH_3CHO$  concentrations with different side  $CO_2$  additions. Figure 20a illustrated that the coupled chemical effects of  $NH_3$  and  $CO_2$  decreased the mole fractions of  $CH_2O$  with the fuel-side  $CO_2$  addition slightly (F1–F9 conditions in Table 2), whereas for the oxidizer side (F10–F18 conditions in Table 2), the coupled chemical effects promoted  $CH_2O$  formation. It could be explained that the chemical effects of  $CO_2$  promoted the formation of  $CH_2O$ , and the coupled chemical effects of  $NH_3$  and  $CO_2$  were mainly affected by the chemical effects of  $CO_2$ , leading to an

**Fig. 20** The Difference of peak mole fractions of  $CH_2O$  and  $CH_3CHO$ . **a**  $CH_2O$ ; **b**  $CH_3CHO$



increase of the mole fraction of  $\text{CH}_2\text{O}$  with the oxidizer-side  $\text{CO}_2$  addition.

Additionally, the chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  on the mole fraction of  $\text{CH}_3\text{CHO}$  were different from those of  $\text{CH}_2\text{O}$ . According to Fig. 20b, it could be found that the chemical effects of  $\text{NH}_3$  promoted the formation of  $\text{CH}_3\text{CHO}$ , meanwhile, the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  further promoted the formation of  $\text{CH}_3\text{CHO}$ , especially when  $\text{CO}_2$  was added to the oxidizer side.

## 4 Conclusions

The chemical kinetic analyses for the chemical effects of  $\text{NH}_3$  with different diluents, in particular the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  in ethylene counter-flow diffusion flames, were investigated in this work. The analyses encompassed several critical aspects, such as flame temperature, major species, typical free radicals, intermediate hydrocarbon products, and oxygenated species. The outcomes of the study led to the following conclusions:

- (1) Regardless of the diluents utilized, the flame temperature and the mole fractions of O, H, OH,  $\text{C}_2\text{H}_2$ ,  $\text{C}_3\text{H}_3$ , A1 were decreased with  $\text{NH}_3$  addition in  $\text{C}_2\text{H}_4/\text{NH}_3$  counter-flow diffusion flames.
- (2) With Ar or He dilution, the chemical effects of  $\text{NH}_3$  promoted the formation of OH,  $\text{C}_2\text{H}_2$ ,  $\text{C}_3\text{H}_3$ , and A1. With replacing Ar with He on the oxidizer side, the high thermal diffusivity of He reduced the flame temperature, and the pathway of A1 generated by small molecules  $\text{C}_3\text{H}_3$  was more easily susceptible to He, leading to the lower concentrations of  $\text{C}_3\text{H}_3$  and A1.
- (3) With fuel-side  $\text{CO}_2$  addition, the coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  increased the flame temperature and the mole fractions of OH,  $\text{C}_2\text{H}_2$ ,  $\text{C}_3\text{H}_3$ , A1. However, with oxidizer-side  $\text{CO}_2$  addition, the coupled chemical effects, which were affected by the chemical effects of  $\text{CO}_2$  significantly, inhibited the flame temperature and the formations of O, H, OH,  $\text{C}_2\text{H}_2$ ,  $\text{C}_3\text{H}_3$ , A1.
- (4) The chemical effects of  $\text{NH}_3$  resulted in a decrease in the mole fraction of  $\text{CH}_2\text{O}$  and an increase in the concentration of  $\text{CH}_3\text{CHO}$ . The coupled chemical effects of  $\text{NH}_3$  and  $\text{CO}_2$  increased the  $\text{CH}_2\text{O}$  concentration with the oxidizer-side  $\text{CO}_2$  addition.

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**Availability of data and materials** Data will be available upon the request for authors.

## Declarations

**Competing interests** The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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