



Gas generation from coal: taking Jurassic coal in the Minhe Basin as an example

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Abstract The gas generation features of coals at different maturities were studied by the anhydrous pyrolysis of Jurassic coal from the Minhe Basin in sealed gold tubes at 50 MPa. The gas component yields (C_1 , C_2 , C_3 , $i-C_4$, $n-C_4$, $i-C_5$, $n-C_5$, and CO_2); the $\delta^{13}C$ of C_1 , C_2 , C_3 , and CO_2 ; and the mass of the liquid hydrocarbons (C_{6+}) were measured. On the basis of these data, the stage changes of $\delta^{13}C_1$, $\delta^{13}C_2$, $\delta^{13}C_3$, and $\delta^{13}CO_2$ were calculated. The diagrams of $\delta^{13}C_1-\delta^{13}C_2$ vs $\ln(C_1/C_2)$ and $\delta^{13}C_2-\delta^{13}C_1$ vs $\delta^{13}C_3-\delta^{13}C_2$ were used to evaluate the gas generation features of the coal maturity stages. At the high maturity evolution stage ($T > 527.6$ °C at 2 °C/h), the stage change of $\delta^{13}C_1$ and the CH_4 yield are much higher than that of CO_2 , suggesting that high maturity coal could still generate methane. When $T < 455$ °C, CO_2 is generated by breaking bonds between carbons and heteroatoms. The reaction between different sources of coke and water may be the reason for the complicated stage change in $\delta^{13}C_{CO_2}$ when the temperature was higher than 455 °C. With increasing pyrolysis temperature, $\delta^{13}C_1-\delta^{13}C_2$ vs $\ln(C_1/C_2)$ has four evolution stages corresponding to the early stage of breaking bonds between carbon and hetero atoms, the later stage of breaking bonds between carbon and hetero atoms, the cracking of C_{6+} and coal demethylation, and the cracking of C_{2-5} . The $\delta^{13}C_2-\delta^{13}C_1$ vs $\delta^{13}C_3-\delta^{13}C_2$ has three evolution stages corresponding to the breaking bonds between carbon and hetero atoms, demethylation and cracking of C_{6+} , and cracking of C_{2-5} .

Keywords Jurassic coal · Pyrolysis · Gas generation · $\delta^{13}C$ · Stage evolution

1 Introduction

The natural gas generated from different origins provides its formation characteristics during its evolution (Behar et al. 1992, 2008, 2010; Wang et al. 2013). Coal-formed gas has been an important field of natural gas and plays an

important role in China's natural gas resources (Dai et al. 2014). The heterogeneity of coal is strong, and the evolution features of coal-formed gas are more complex than those of other source rocks (Sun et al. 2013). The kinetics of hydrocarbon generation extend the hydrocarbon generation of coal under laboratory conditions to geologic history (Butala et al. 2000; Ping'an et al. 2009; Shuai et al. 2006), which simplifies the gas evolution of the coal. $\delta^{13}C$ is one of the most important properties of natural gas. The $\delta^{13}C$ of coal-formed methane has obvious evolution stage features (Cramer 2004; Cramer et al. 1998; Liu and Xu 1999), and the $\delta^{13}C$ of natural gas could be used to trace the gas origin (Schoell 1980; Song and Xu 2005). The process of gas formation and evolution could be reflected by the $\delta^{13}C$ relationship of different carbon numbers (Chung et al. 1988; Peng et al. 2009). The diagram of

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$\delta^{13}\text{C}_2\text{-}\delta^{13}\text{C}_1$ versus $\delta^{13}\text{C}_3\text{-}\delta^{13}\text{C}_2$ could reflect the maturity of natural gas (Jenden et al. 1993), and the diagrams of $\ln(C_2/C_3)$ vs $\ln(C_1/C_2)$ and $\delta^{13}\text{C}_i\text{-}\delta^{13}\text{C}_j$ vs $\ln(C_i/C_j)$ can be used to distinguish the gas origin (Prinzhofer and Huc 1995); these indicators are largely associated with thermal evolution (Tian 2006).

In recent years, there has been increasing attention on the CO_2 generated during the thermal evolution of coal (Fu et al. 2019a; Killops et al. 1996; Kotarba and Lewan 2004; Lewan and Kotarba 2014; Shuai et al. 2013a, b). CO_2 could be generated from organic matter at any maturity stage (Shuai et al. 2013b); at low maturity, CO_2 could be generated from the cracking of kerogen itself, and the disproportionation between organic matter and water could generate CO_2 at the high maturity stage (Seewald 2003; Seewald et al. 1998). The $\delta^{13}\text{C}$ of CO_2 in natural gas could be used for gas source contrast (Song and Xu 2005), and some post-reformation of natural gas can be reflected by $\delta^{13}\text{CO}_2$ (Rice 1993; Zhang et al. 2004).

The evolution of coal-formed gas abundance and the $\delta^{13}\text{C}$ of gas can be measured by pyrolysis experiments (Behar et al. 1995; Hill et al. 2007; Lewan et al. 1985). Coal has a favorable gas generation ability and low oil generation potential (Hill et al. 2003; Shuai et al. 2006), and because of its molecular sieve nature and chemical adsorption property, liquid hydrocarbons can be generated when $R_o\% = 0.7$, but oil expulsion cannot occur (Cook 1988; Johnston et al. 1991). Therefore, a closed system simulation experiment could reflect the gas generation process from coal, and anhydrous pyrolysis in sealed gold tubes under pressure could simulate the geological condition very well (Behar et al. 2008; Hill et al. 2007; Tang et al. 1996).

Previous hydrocarbon-generation kinetics research on Jurassic coal from the Minhe Basin shows that the mean values of the activation energies of CH_4 and C_{1-5} are 64.55 kcal/mol and 63.93 kcal/mol, respectively, with a frequency factor of $1.0 \times 10^{14} \text{ s}^{-1}$ (Fu et al. 2019b). However, the stage evolution characteristics of gas generation have not been studied. In this study, the anhydrous pyrolysis of Jurassic coal from the Minhe Basin in sealed gold tubes was simulated. The gas component yields (C_1 , C_2 , C_3 , *i*- C_4 , *n*- C_4 , *i*- C_5 , *n*- C_5 , and CO_2); the $\delta^{13}\text{C}$ of C_1 , C_2 , C_3 , and CO_2 ; and the mass of liquid hydrocarbons (C_{6+}) were measured. Then, the stage $\delta^{13}\text{C}$ values of C_1 , C_2 , C_3 , and CO_2 were calculated, and the diagrams of $\delta^{13}\text{C}_1\text{-}\delta^{13}\text{C}_2$ versus $\ln(C_1/C_2)$ and $\delta^{13}\text{C}_2\text{-}\delta^{13}\text{C}_1$ versus $\delta^{13}\text{C}_3\text{-}\delta^{13}\text{C}_2$ were obtained to study the gas evolution of coal.

2 Experimental

2.1 Sample and closed system pyrolysis

The immature Jurassic coal used in this study was from the Minhe Basin, Gansu Province, China (Fig. 1), and the basic geochemical characterization of the sample is listed in Table 1.

The coal was pulverized via a 100 mesh, and no other chemical treatment was conducted. The pyrolysis experiments were conducted in sealed gold tubes (40 mm \times 5 mm). The sample (15–60 mg) was loaded in a gold tube with one end welded closed, and the air was replaced by argon. The open end was then welded closed by TIG (Pulse arc welding) with the closed end protected in room temperature water. The samples in sealed gold tubes were heated in one furnace in 12 separated stainless steel autoclaves. To avoid the influence of phase differentiation, the experiment was conducted at a constant pressure of 50 MPa, in which the fluid phase is basically in a single phase (Fu et al. 2019a, b). Two series of experiments were conducted, and the gold tubes were heated for 10 h from room temperature to 250 °C and then heated to 600 °C with heating rates of 20 °C/h and 2 °C/h. Additional descriptions of the experimental procedure can be found in (Pan et al. 2007; Shuai et al. 2013b; Wang et al. 2013).

2.2 Gas analysis

After the pyrolysis experiment, the gold tube was punctured in a closed system and connected to an Agilent 7890A gas chromatograph (GC) that has a Wasson ECE module for analyzing the gas composition (C_{1-5} , CO_2) using the external standard method to calculate the quantities of each gas component. The GC employed an HP-AL/S capillary column (25 m \times 0.32 mm \times 0.8 μm) and used helium as the carrier gas. The column temperature was programmed from 60 °C (held for 3 min) to 190 °C (held for 3 min) at 25 °C/min.

2.3 Stable carbon isotope analysis

The $\delta^{13}\text{C}$ levels of C_1 , C_2 , C_3 , and CO_2 analysis were conducted on an Isoprime 100 mass spectrometer that interfaced an Agilent 6890 GC. The GC was equipped with a CP-Poraplot Q column (27.5 m \times 0.32 mm \times 10 μm), and helium was used as the carrier gas. The column temperature was programmed from 50 °C (held for 3 min) to 190 °C (held for 5 min) at 25 °C/min. The $\delta^{13}\text{C}$ of each sample was measured twice, and the average deviation was less than 0.3‰.

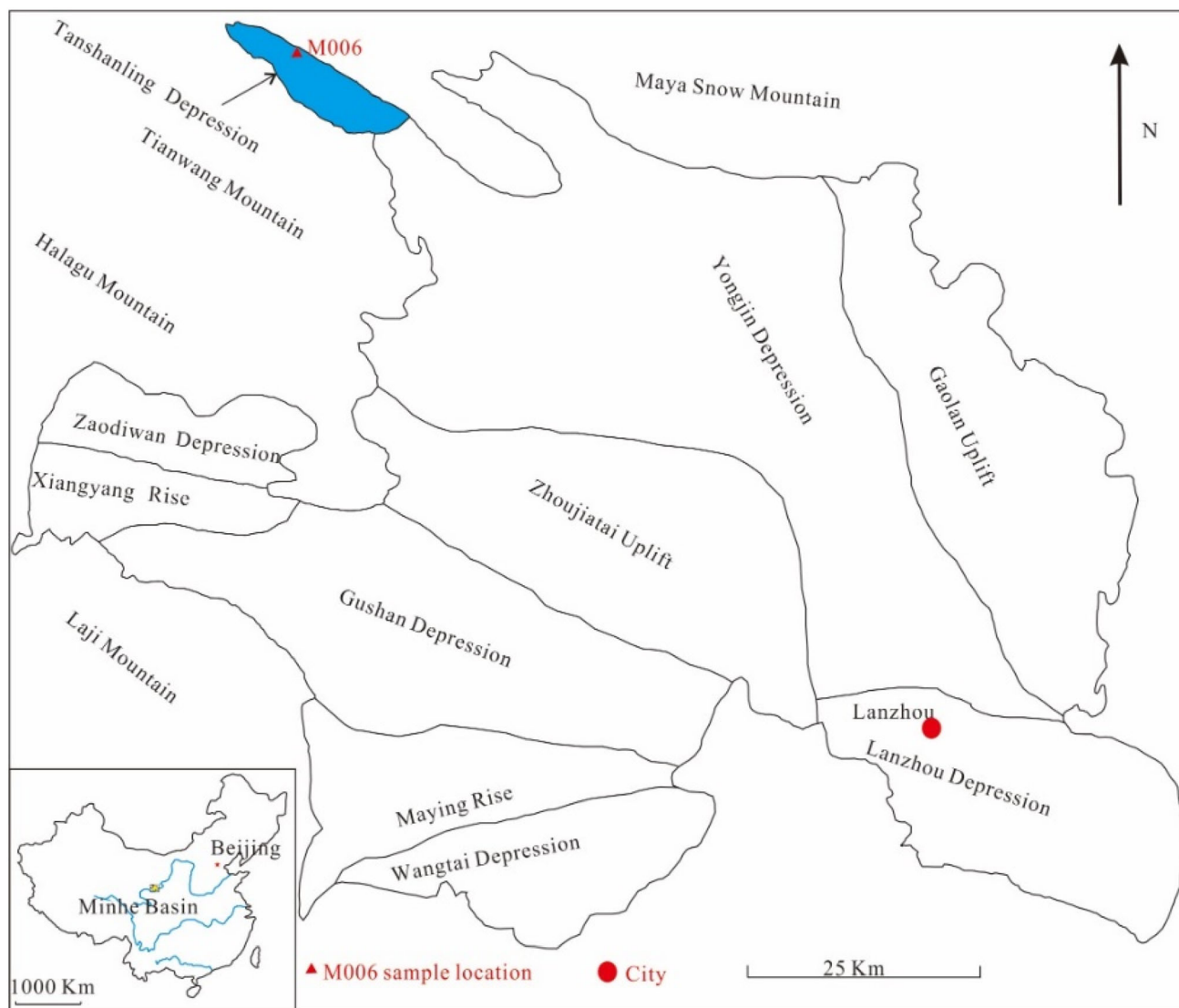


Fig. 1 Sample location

Table 1 Geochemical characterization of the sample in this study

Sample	TOC ^a (%)	T _{max} ^b (°C)	I _H (mg/ g) ^c	I _O (mg/ g) ^d	S ₁ (mg/ g) ^e	S ₂ (mg/ g) ^f	S ₃ (mg/ g) ^g
M006	75	426	183.13	4.11	4.38	143.76	3.23

^aTotal organic carbon

^bTemperature of maximum release of hydrocarbons from cracking of kerogen

^cHydrogen index

^dOxygen index

^eAmount of free hydrocarbons

^fAmount of hydrocarbons generated through thermal cracking

^gAmount of CO₂ pyrolysis of kerogen

2.4 C₆₊ analysis

The C₆₊ composition was separated to C₆₋₁₄ and C₁₄₊ for analysis. After the gas composition was analyzed, the C₆₋₁₄ liquids were collected by a liquid nitrogen cold trap (4 mL, quartz bottle) (Behar et al. 1995) and injected with 3 mL of n-hexane. Then, the gold tube was cut into pieces and put into the bottle to ensure that the C₆₊ liquids could be dissolved completely. Deuterated-24-alkanes were used as the internal standard to determine the quantities of the liquids. The analysis was conducted on an Agilent 7890A GC that employed a DM-5 capillary column (30 mm × 0.32 mm × 0.25 μm) and used helium as the carrier gas. The initial oven temperature was 40 °C and held for 5 min, after which the oven was heated to 290 °C with a heating rate of 4 °C/min and held at 290 °C for 15 min. The C₁₄₊

was ultrasonically extracted by dichloromethane and weighed.

3 Results

3.1 Liquid (C₆₊) yield

The yields of C₆₊ should be the sum of C₆₋₁₄ and C₁₄₊. Table 2 and Fig. 2a show the cumulative yields of the liquid hydrocarbons (C₆₊) in the experiments. As Fig. 2a shows, the yields of C₆₊ increased rapidly at low temperature ($T < 410$ °C), and the maximum yield was 78.17 mg/g TOC (20 °C/h, 406.9 °C). The yield began to decrease rapidly when the temperature > 410 °C because of cracking.

3.2 Gas yields

The yields of C₁, C₂, C₃, C₄, C₅, and CO₂ generated from coal pyrolysis are shown in Fig. 2 and Table 2. As a whole, C₂₋₅ (Fig. 2b) peaked at 431 °C (2 °C/h) and 478 °C (20 °C/h), which is close to the end of the C₆₊ liquids cracking. The volumetric productivities of C₂, C₃, C₄ and

C₅ were in descending order, and the relationship with temperature was similar. However, the cracking temperature was different and decreased with increasing carbon number; in addition, the cracking temperature was different at different heating rates, which manifested as the temperature became lower during the slow heating rate than during the rapid heating rate.

The yields of methane were low before 410 °C and increased rapidly after 410 °C, which was close to the cracking temperature of the C₆₊ liquids. The maximum yield of methane was 257.35 mL/g TOC (599.3 °C, 2 °C/h), which was much higher than that of all the other gases. At the same temperature, the gas yield during the slow heating rate was higher than during the rapid heating rate, which was the result of the complementary relationship between time and temperature on the chemical kinetics (Connan 1974).

CO₂ is the most important nonhydrocarbon gas of the coal thermal maturity process (Shuai et al. 2013b; Tang et al. 1996). Figure 2h shows that the yield of CO₂ was significant at 336 °C and much higher than that of the hydrocarbon gases. The yield of methane exceeded that of CO₂ when the temperature was higher than 455 °C (20 °C/h) and 431 °C (2 °C/h), and the maximum CO₂ was

Table 2 Yields of gases and their $\delta^{13}\text{C}$ value and liquid hydrocarbon generated by pyrolysis experiment

T(°C)	Rate (°C/h)	CO ₂	C ₁	C ₂	C ₃	<i>i</i> -C ₄ (mL/g)	<i>n</i> -C ₄	<i>i</i> -C ₅	<i>n</i> -C ₅	C ₂₋₅	C ₆₊ (mg/g)	$\delta^{13}\text{C}_1$ (‰)	$\delta^{13}\text{C}_2$ (‰)	$\delta^{13}\text{C}_3$ (‰)	$\delta^{13}\text{C}_{\text{CO}_2}$ (‰)
334.8	20	10.41	0.44	0.04	0.01	0.02	–	–	–	0.08	8.86	– 31.58	–	–	– 24.03
358.9	20	18.34	1.74	0.31	0.11	0.05	0.01	0.01	–	0.49	11.47	– 32.52	– 27.69	– 26.23	– 22.27
382.8	20	26.41	4.79	1.45	0.63	0.16	0.06	0.04	0.01	2.35	30.09	– 35.21	– 29.05	– 26.59	– 21.08
406.9	20	36.07	12.37	4.48	2.00	0.28	0.25	0.08	0.04	7.12	78.17	– 37.39	– 28.23	– 25.67	– 20.88
431	20	42.14	25.43	8.12	3.31	0.49	0.48	0.21	0.09	12.69	43.48	– 37.12	– 27.23	– 24.92	– 20.69
454.9	20	47.71	48.12	12.37	4.42	0.59	0.60	0.18	0.09	18.26	23.64	– 35.42	– 25.92	– 23.79	– 20.60
478.7	20	50.18	77.78	14.54	3.53	0.61	0.26	0.08	0.01	19.03	18.94	– 33.58	– 24.48	– 21.37	– 21.41
503.0	20	54.69	116.99	12.53	1.28	0.19	0.01	–	–	14.02	13.94	– 31.38	– 20.36	– 13.64	– 21.26
525.0	20	56.92	147.03	7.53	0.22	0.01	–	–	–	7.76	7.81	– 29.92	– 15.23	–	– 20.85
544.0	20	60.72	167.92	3.57	0.02	–	–	–	–	3.59	6.02	– 29.11	– 9.60	–	– 21.55
562.0	20	68.46	187.78	1.62	–	–	–	–	–	1.62	5.65	– 27.76	–	–	– 21.37
585.0	20	73.09	205.67	0.88	–	–	–	–	–	0.88	5.65	– 26.96	–	–	– 22.33
334.8	2	21.29	2.32	0.48	0.18	0.06	0.01	0.01	–	0.75	21.01	– 33.80	– 28.44	– 26.28	– 21.90
358.7	2	33.33	6.35	2.06	0.86	0.14	0.07	0.03	0.01	3.16	57.19	– 35.98	– 29.18	– 26.25	– 20.74
383.5	2	41.36	15.95	5.50	2.28	0.27	0.26	0.07	0.04	8.41	56.89	– 37.71	– 27.89	– 25.16	– 20.90
407.2	2	48.85	35.92	10.01	3.68	0.37	0.45	0.08	0.06	14.66	26.92	– 36.50	– 26.44	– 24.49	– 21.03
431.2	2	52.08	63.39	13.32	3.80	0.34	0.35	0.04	0.03	17.88	12.96	– 34.73	– 25.23	– 22.66	– 20.99
455.3	2	60.60	105.04	13.41	1.63	0.07	0.04	–	–	15.14	9.88	– 31.87	– 22.07	– 16.98	– 20.63
479.0	2	63.35	141.84	7.97	0.20	–	–	–	–	8.18	6.65	– 30.42	– 15.89	–	– 20.81
503.3	2	69.83	174.00	2.29	0.01	–	–	–	–	2.30	9.29	– 28.60	– 7.39	–	– 21.43
527.6	2	71.25	197.77	0.90	–	–	–	–	–	0.91	8.95	– 27.27	–	–	– 21.36
551.8	2	83.62	214.18	0.68	–	–	–	–	–	0.68	8.01	– 26.65	–	–	– 22.46
575.8	2	96.71	237.50	0.36	–	–	–	–	–	0.37	7.12	– 26.12	–	–	– 23.34
599.3	2	112.14	257.35	0.42	–	–	–	–	–	0.42	4.25	– 26.26	–	–	– 22.99

“–” indicates not detected

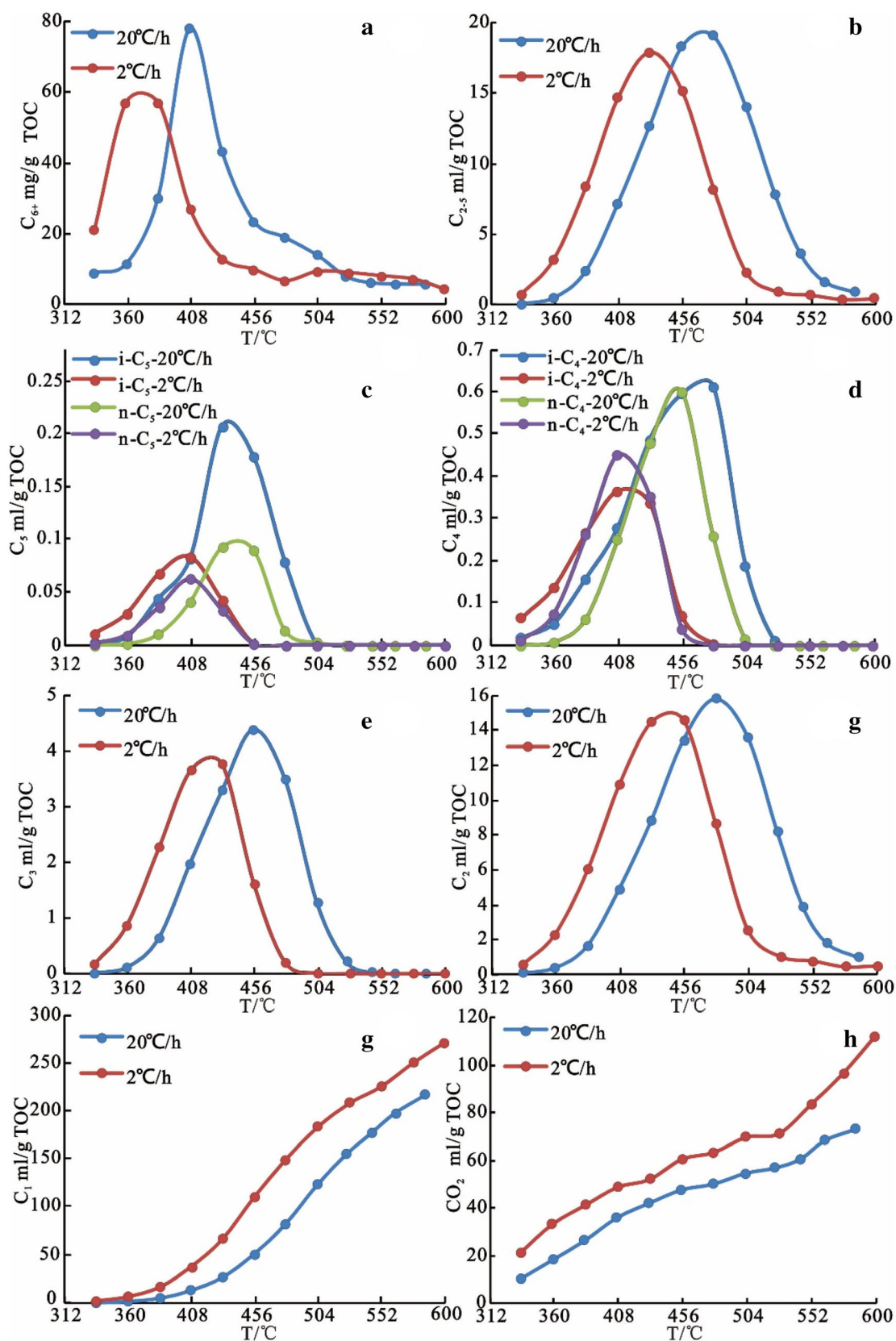


Fig. 2 The C₆₊ yields of (a), C₂₋₅ (b), C₅ (c), C₄ (d), C₃ (e), C₂ (f), C₁ (g), and CO₂ (h) during the pyrolysis experiments

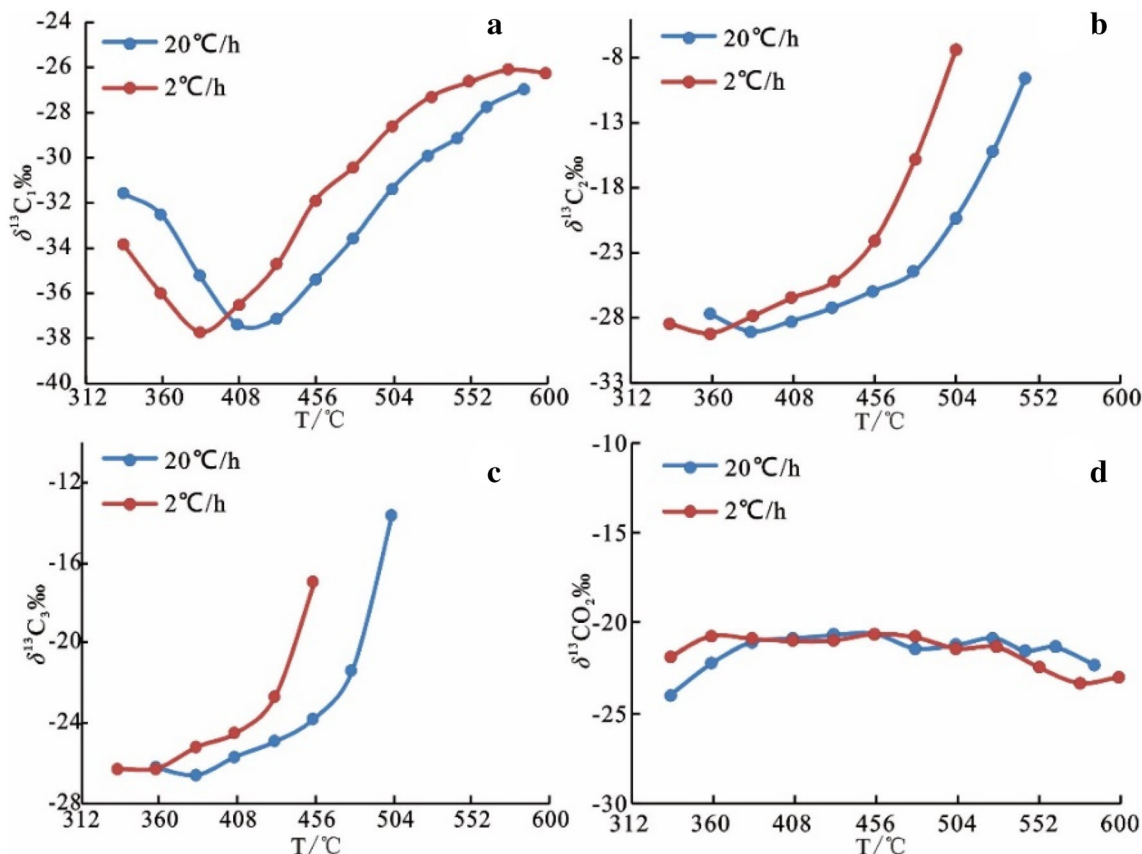
Table 3 XRD text result of sample

Mineral	Content (%)	Mineral	Content (%)
Quartz	7.19	Dolomite	0.68
Calcite	2.05	Gypsum	1.09
montmorillonite	12.79	Pyrite	3.14
Illite	35.00	Siderite	0.75
Kaolinite	14.24	Orthoclase	1.01
Chlorite	19.03	Hematite	1.46
Anorthoclase	1.57		

112.13 mL/g TOC (599.3 °C, 2 °C/h). The XRD results (Table 3) indicated that the sample contains very small amounts of carbonate minerals, and the detection of liquid HCl showed the same results. The carbonate minerals contained in the sample could not generate such a large amount of CO₂, which means that the CO₂ was mainly from an organic origin.

3.3 The $\delta^{13}\text{C}$ of gases

The $\delta^{13}\text{C}$ values of C₁, C₂, C₃, and CO₂ are shown in Fig. 3 and Table 2. The $\delta^{13}\text{C}$ of C_{1–3} decreased with increasing pyrolysis temperature and then began to enrich ¹³C, manifesting as $\delta^{13}\text{C}_1 < \delta^{13}\text{C}_2 < \delta^{13}\text{C}_3$ at the same temperature and heating rate. Taking 2 °C/h as an example, the $\delta^{13}\text{C}_1$ decreased over the range of 334.8–383.5 °C and began to enrich the ¹³C after 383.5 °C and the lightest $\delta^{13}\text{C}_1$ was −37.71‰. Many other pyrolysis experiments of kerogen and crude oil samples have similar changes (Tang et al. 2000; Tian et al. 2007; Wang et al. 2013; Xiong et al. 2004). The $\delta^{13}\text{C}$ of CO₂ ranged from −24.03‰ to 20.62‰, and this is much less than that of hydrocarbon gases and is different from the report of Shuai et al. (2013b), showing that CO₂ became enriched in ¹³C with increasing temperature but increased to −20.74‰ at 358.7 °C and then fluctuated between −20.63‰ and −21.03‰ to 479.0 °C; in addition, with increasing temperature, it became lighter after 479.0 °C.

**Fig. 3** $\delta^{13}\text{C}$ of C₁, C₂, C₃, and CO₂ during the pyrolysis experiment

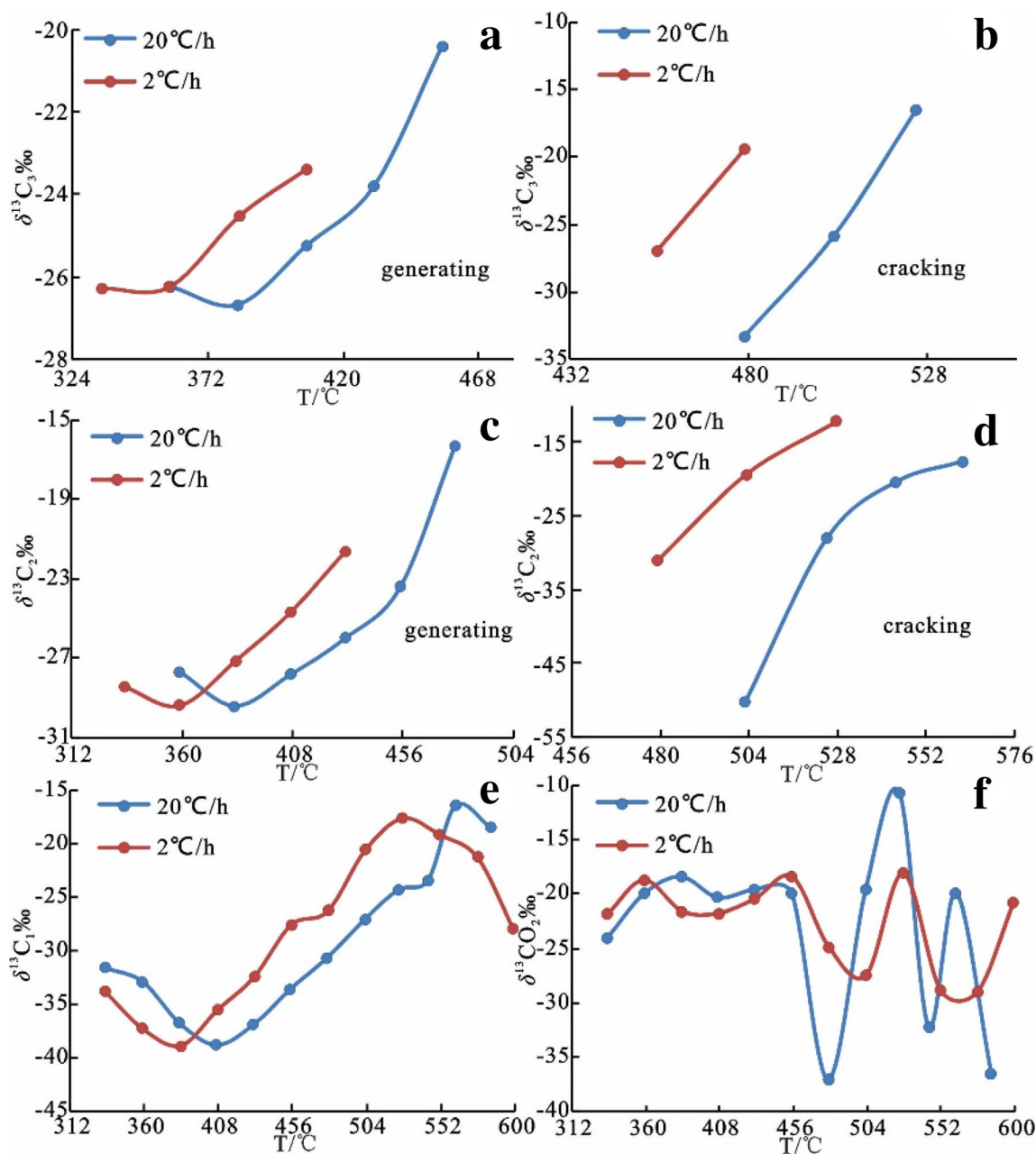


Fig. 4 The different stage $\delta^{13}\text{C}$ values of C_1 , C_2 , C_3 , and CO_2 during the pyrolysis experiment

4 Discussion

4.1 Stage $\delta^{13}\text{C}$ values of C_1 , C_2 , C_3 , and CO_2

The instantaneous changes in $\delta^{13}\text{C}$ could not be obtained because of the closed pyrolysis system. To solve this problem, the following formula was used to calculate the stage value of $\delta^{13}\text{C}$ according to the law of isotopic conservation and based on the gas yields and $\delta^{13}\text{C}$ (Shuai et al. 2013b):

$$\delta^{13}\text{C}'_{T_i} = (\delta^{13}\text{C}_{T_i} \times V_{T_i} - \delta^{13}\text{C}_{T_{i-1}} \times V_{T_{i-1}}) / (V_{T_i} - V_{T_{i-1}}) \tag{1}$$

where, $\delta^{13}\text{C}'_{T_i}$ is the stage value of $\delta^{13}\text{C}$ from temperature T_{i-1} to T_i ; $\delta^{13}\text{C}_{T_i}$ and $\delta^{13}\text{C}_{T_{i-1}}$ are the cumulative $\delta^{13}\text{C}$ values of gases at temperatures T_i and T_{i-1} , respectively; and V_{T_i} and $V_{T_{i-1}}$ are the cumulative volumetric yields of gases at temperature T_i and T_{i-1} , respectively.

The stage $\delta^{13}\text{C}$ values of C_1 , C_2 , C_3 , and CO_2 are shown in Fig. 4. Ethane and propane are generated and cracked during pyrolysis, so $\delta^{13}\text{C}'_{T_i}$, calculated by Eq. (1), can be divided into two processes. There is a certain temperature

overlap between ethane and propane at the end of the formation and at the beginning of the cracking (Shuai et al. 2006; Tian 2006), so the calculated values that were close to the temperature when cracking began were discarded. As shown in Fig. 4, with increasing pyrolysis temperature, the stage $\delta^{13}\text{C}$ values of C_2 and C_3 first decreased and then increased during the generation stage. During the cracking processes, the light carbon ethane and propane were cracked prior because the bond energy of $^{12}\text{C}\text{--}^{13}\text{C}$ is higher than that of $^{12}\text{C}\text{--}^{12}\text{C}$ (Arneht and Matzigkeit 1986; Stevenson et al. 1948; Tang et al. 2000). Therefore, the cumulative values of $\delta^{13}\text{C}_2$ and $\delta^{13}\text{C}_3$ in Fig. 3 began to increase when the cracking temperature was reached.

The stage $\delta^{13}\text{C}$ value of C_1 is significantly different from its cumulative value. Cramer (2004) explained the evolution of the $\delta^{13}\text{C}$ value of coal-generated methane according to kinetics and divided methane generation into the following four reaction stages: (1) cleavage of heteroatoms, (2) demethylation reactions, (3) second cracking of long-chain alkanes and cyclic compounds generated, and (4) polycondensation reactions. Taking $2\text{ }^\circ\text{C/h}$ as an example, with the increase of pyrolysis temperature, the stage $\delta^{13}\text{C}_1$ value decreased to -38.85‰ at $383.5\text{ }^\circ\text{C}$, which means it was close to the end of the reaction stage (1) (Cramer 2004; Liao et al. 2007). After that, the stage value of $\delta^{13}\text{C}_1$ began to increase, and the peak value of -17.59‰ was reached at $527.6\text{ }^\circ\text{C}$. This stage corresponded to the second cracking of liquid hydrocarbon (C_{6+}) and wet gas (C_{2-5}) one after another (Fig. 2a, b), which reflects that reactions stage (2) and (3) occurred (Cramer 2004). Then, the stage value of $\delta^{13}\text{C}_1$ started to decrease with increasing temperature, and the yield continued to increase which corresponding to the reaction stage (4). However, the changes in $\delta^{13}\text{C}_2$ and $\delta^{13}\text{C}_3$ (Figs. 3, 4) and their remaining amounts (Fig. 2) showed that the cracked gases were almost complete and that $\delta^{13}\text{C}$ became heavier, which means that the methane generated at this stage came from not only the cracking of C_{2-5} but also other reactions that may be the main source of methane. The reaction between water and coke in the higher evolution stage could generate some of the CH_4 , but as Eq. (2) below shows



The gas generation yields of CO_2 and CH_4 of this evolution stage should be equal; however, as Table 2 shows, the increase in CH_4 is much higher than that in CO_2 . Therefore, there must be another origin of CH_4 . Cramer (2004) points out that the polycondensation reaction is the reason that $\delta^{13}\text{C}_1$ decreases during this stage and that coal has gas generation potential at this stage.

The stage $\delta^{13}\text{C}$ value of CO_2 was complex and changed between -37.04‰ and -10.67‰ , and it is generally

believed that the $\delta^{13}\text{CO}_2$ of an organic origin is less than -10‰ (Dai et al. 1996; Wycherley et al. 1999); in addition, the calculated stage $\delta^{13}\text{C}$ value of CO_2 shows that the CO_2 in the experiment was of an organic origin and that the XRD result (Table 3) also supported this view. Shuai et al. (2013b) suggest that the $\delta^{13}\text{C}$ of organic origin CO_2 could be as high as 18‰ . However, in this paper, the data do not support this conclusion, which may be due to the complex composition of coal. The stage $\delta^{13}\text{C}$ value of CO_2 changed smoothly before $455\text{ }^\circ\text{C}$ (remaining at approximately -20‰), which was significantly higher than the stage $\delta^{13}\text{C}$ value of methane at the same stage. This is because during this stage, the CO_2 is mainly sourced from the cleavage of the heteroatom reaction of coal (Seewald et al. 1998), and the carbon that is attached to the heteroatom is more enriched in ^{13}C than the aliphatic side chains (Cheng et al. 2009). At the high maturity stage, CO_2 is generated from the reaction between H_2O and organic matter (Lewan 1997; Seewald et al. 1998). Because of anhydrous pyrolysis, H_2O may originate from the pyrolysis of coal or from the bond water in clay minerals (Wang et al. 2013). When the temperature was higher than $455\text{ }^\circ\text{C}$, the stage $\delta^{13}\text{C}$ value of CO_2 changed substantially, which may be related to the different causes of coke (cracking of aromatization carbon or liner carbon) reacting with H_2O . In fact, as the experimental temperature increases, the number of free radicals in the reaction system increases accordingly. The generated CO_2 should result of the reaction of oxygen free radicals and carbon free radicals. The oxygen free radicals and carbon free radicals here are from the cracking of H_2O and coal, respectively. At the same time, we believe that the production of C radicals is mainly affected by temperature and pressure, and the isotope fractionation process is more complicated, which directly leads to the complex characteristics of the $\delta^{13}\text{C}$ value of CO_2 .

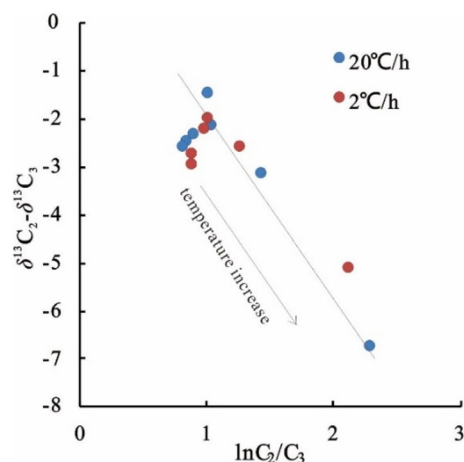


Fig. 5 $\delta^{13}\text{C}_2\text{--}\delta^{13}\text{C}_3$ vs. $\ln \text{C}_2/\text{C}_3$

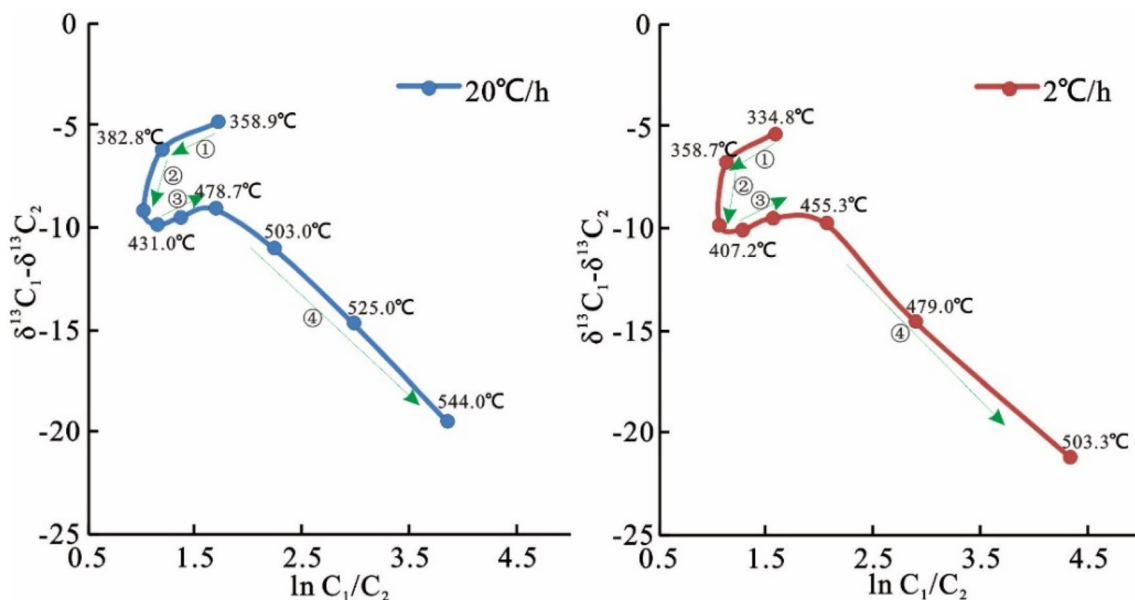


Fig. 6 $\delta^{13}C_1 - \delta^{13}C_2$ vs $\ln C_1/C_2$ ((1) the increase ratio of ethane was higher than that of methane, and the isotope fractionation effect of methane was higher than that of ethane; (2) the end of the cleavage heteroatom reaction, where C_1/C_2 remained almost unchanged and $\delta^{13}C_1 - \delta^{13}C_2$ decreased rapidly; (3) both the methane and ethane yields increased because of C_{6+} undergoing cracking; (4) the ethane begins to crack)

4.2 $\delta^{13}C_1 - \delta^{13}C_j$ vs $\ln C_i/C_j$

The $\delta^{13}C$ of hydrocarbon gases has a good correlation with thermal maturity and source rock (Dai and Qi 1989; Schoell 1983), and the gas composition is very sensitive to thermal maturity (Wang et al. 2013). Therefore, the $\delta^{13}C_1 - \delta^{13}C_j$ vs $\ln C_i/C_j$ diagram can be used to indicate the thermal maturity and source rock of natural gas (Hill et al. 2003; Prinzhofer and Huc 1995; Tian et al. 2010). The $\delta^{13}C_2 - \delta^{13}C_3$ vs $\ln C_2/C_3$ diagram based on the pyrolysis experimental data (Fig. 5) shows a significant feature of kerogen pyrolysis gas (Prinzhofer and Huc 1995), which is characteristic of coal.

The $\delta^{13}C_1 - \delta^{13}C_2$ versus $\ln C_1/C_2$ diagram could be used to reflect the maturity of natural gas, the leakage of natural gas and the mixing of thermogenic gas and biogenic gas (Jenden et al. 1993; Prinzhofer and Huc 1995). The closed system pyrolysis experiment could exclude the influences of leakage and biogenic gas, which should only be correlated with the thermal maturity and the sample. The $\delta^{13}C_1 - \delta^{13}C_2$ versus $\ln C_1/C_2$ diagram based on the pyrolysis experimental data (Fig. 6) shows obvious stage changes. Taking 2 °C/h as an example, the first stage was 334.8–358.7 °C, and C_1/C_2 decreased with increasing temperature, which means that the increasing ratio of ethane was higher than that of methane (Wang et al. 2013). The $\delta^{13}C_1 - \delta^{13}C_2$ decreased slightly, which was possibly because both methane and ethane were generated from cleavage of the heteroatom side chain, and the isotope fractionation effect of methane was higher than that of

ethane. The second stage was from 358.7 to 407.2 °C, corresponding to the end of the cleavage heteroatom reaction. The C_1/C_2 almost remained unchanged, and the $\delta^{13}C_1 - \delta^{13}C_2$ decreased rapidly because of high hereditability from the source rock of ethane (James 1983; Xie et al. 1999). The next stage was from 407.2 to 455.3 °C, both the methane and ethane yields were increased because of the cracking of C_{6+} (Fig. 2) during this interval, and the $\delta^{13}C_1$ and $\delta^{13}C_2$ were also increased. C_1/C_2 increased, which means that the increase ratio of methane was higher than that of ethane, and the $\delta^{13}C_1 - \delta^{13}C_2$ increased slightly, showing that the degree of increasing $\delta^{13}C_1$ heaviness was larger than that of $\delta^{13}C_2$. When the temperature was higher than 455.3 °C, ethane began to crack (Fig. 2), and C_1/C_2 increased rapidly with decreasing $\delta^{13}C_1 - \delta^{13}C_2$.

4.3 $\delta^{13}C_3 - \delta^{13}C_2$ vs $\delta^{13}C_2 - \delta^{13}C_1$

The $\delta^{13}C_3 - \delta^{13}C_2$ and $\delta^{13}C_2 - \delta^{13}C_1$ values decrease with increasing thermal maturity (Jenden et al. 1993; Prinzhofer and Huc 1995), so the $\delta^{13}C_3 - \delta^{13}C_2$ vs $\delta^{13}C_2 - \delta^{13}C_1$ diagram can be used to reflect the maturity of natural gas (Jenden et al. 1993). However, many simulation experiments show the opposite change (Guo et al. 2009, 2011; Tian 2006). The indexes above largely depend on the maturity of natural gas (Tian 2006). As Fig. 7 shows, in this experiment, the $\delta^{13}C_3 - \delta^{13}C_2$ vs $\delta^{13}C_2 - \delta^{13}C_1$ diagram shows obvious stage changes. Taking 2 °C/h as an example, when the temperature was lower than 383.5 °C, the $\delta^{13}C_3 - \delta^{13}C_2$ increased slightly from 2.16‰ to 2.94‰, and

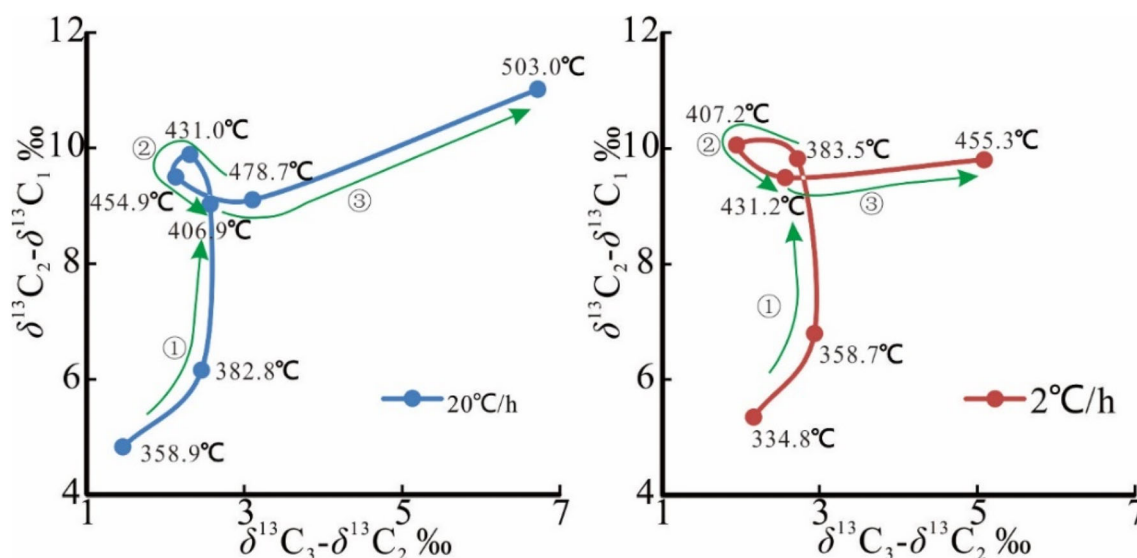


Fig. 7 $\delta^{13}\text{C}_3-\delta^{13}\text{C}_2$ vs $\delta^{13}\text{C}_2-\delta^{13}\text{C}_1$ ((1) $\delta^{13}\text{C}_1$ decreased, but $\delta^{13}\text{C}_2$ first decreased and then increased, and $\delta^{13}\text{C}_3$ remained almost unchanged; (2) the variations in $\delta^{13}\text{C}_1$, $\delta^{13}\text{C}_2$ and $\delta^{13}\text{C}_3$ were basically the same, and the main sources of these gases were generated from C_{6+} cracking; (3) propane cracked before ethane)

the $\delta^{13}\text{C}_2-\delta^{13}\text{C}_1$ increased rapidly from 5.36‰ to 9.82‰. This is because during this stage, $\delta^{13}\text{C}_1$ decreased, but $\delta^{13}\text{C}_2$ first decreased and then increased, and $\delta^{13}\text{C}_3$ remained almost unchanged (Figs. 2, 3). Then, when the temperature was between 383.5 and 431.2 °C, the $\delta^{13}\text{C}_3-\delta^{13}\text{C}_2$ first decreased and then increased, changing over the range of 2‰ to 3‰, and the $\delta^{13}\text{C}_2-\delta^{13}\text{C}_1$ remained almost unchanged. This result indicates that the variations in $\delta^{13}\text{C}_1$, $\delta^{13}\text{C}_2$ and $\delta^{13}\text{C}_3$ were basically the same, and the main sources of these gases were the same during this stage. In contrast to Fig. 2, we conclude that the cracking of C_{6+} was the main source of these gases. The last stage was from 431.2 to 455.3 °C, where $\delta^{13}\text{C}_2-\delta^{13}\text{C}_1$ remained at approximately 10‰ and $\delta^{13}\text{C}_3-\delta^{13}\text{C}_2$ increased rapidly from 1.95‰ to 5.08‰ because of propane undergoing cracking before ethane.

5 Conclusions

Anhydrous pyrolysis experiments were conducted in sealed gold tubes with Jurassic coal from the Minhe Basin. The hydrocarbon composition and CO_2 yields and the $\delta^{13}\text{C}$ of gas compositions were obtained. The following conclusions were drawn:

The stage $\delta^{13}\text{C}$ value of methane shows a change trend of the “S” type that first decreased, then increased and finally decreased. The stage $\delta^{13}\text{C}$ values of ethane and propane first decreased and then increased during the generating stage and became enriched in ^{13}C during the cracking stage because the bond energy of $^{12}\text{C}-^{13}\text{C}$ was higher than that of $^{12}\text{C}-^{12}\text{C}$. The stage $\delta^{13}\text{C}$ value of CH_4

decreased when $T > 520$ °C, but the $\delta^{13}\text{C}$ values of cracked ethane and propane increased, which proved that coal still had the potential to generate CH_4 at high maturity. The stage $\delta^{13}\text{C}$ value of CO_2 changes when $T > 455$ °C since the difference caused coke to be reacted with H_2O .

According to the diagram of $\delta^{13}\text{C}_1-\delta^{13}\text{C}_2$ versus $\ln C_1/C_2$ and $\delta^{13}\text{C}_3-\delta^{13}\text{C}_2$ versus $\delta^{13}\text{C}_2-\delta^{13}\text{C}_1$, five stages of coal gas generation could be determined: (1) early stage of heteroatom cleavage reaction, (2) later stage of heteroatom cleavage reaction, (3) demethylation reaction and second cracking of C_{6+} , (4) cracking of wet gases (C_{2-5}), and (5) polycondensation reaction.

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