**RESEARCH**



# **Environmental risk assessment of industrial byproduct gypsum utilized for flling abandoned mines**

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#### **Abstract**

In response to the basic policy of green and low-carbon circular development to solve resource, environmental and ecological problems, gypsum is considered to be a flling material for mine backflling. To explore the potential risks of gypsum to the groundwater environment due to the backflling of abandoned mines, a sequential batch leaching experiment was carried out in this paper, which used three types of industrial waste gypsum, namely, phosphorus gypsum (PG), titanium gypsum (TG) and fue gas desulfurization gypsum (FGDG). COMSOL Multiphysics 5.4 software was used to simulate and solve the migration process of the leached metal elements in the mine foor when these three gypsum types were used as flling materials to observe the concentration distributions and difusion distances of the metal elements from these three gypsum types in the mine foor. The results show that (1) during repeated contact of the three types of industrial waste gypsum with the leaching medium, the pH levels changed, and the changes in pH afected the leaching patterns for the heavy metal elements in the gypsum. (2) Based on the concentrations of the metal elements that were leached from the three types of gypsum, it can be determined that these three types of gypsum are not classifed as hazardous solid wastes, but they cannot be ruled out with regard to their risk to the groundwater environment when they are used as mine flling materials. (3) When the three types of gypsum are used as flling materials, the concentration distributions of the metal elements and their migration distances all exhibit signifcant changes over time. The concentration distributions, difusion rates and migration distances of the metal elements from the diferent gypsum types are afected by their initial concentrations in the leachate. The maximum migration distances of Zn in the foor from the PG, FGDG and TG are 8.2, 8.1 and 7.5 m, respectively.

**Keywords** Industrial solid waste gypsum · Coal mine back-flling · Leaching of metal elements · Patterns of migration

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# **1 Introduction**

In China, metal or nonmetal mineral assets have a large outputs and reserves, which are an important pillar of national economic and social development. Reasonable flling and governance of the mined-out areas in mines have become a prerequisite for the green mining of mineral resources. Filling mines has become a focus of the government's attention to the control object. Due to the large amounts of accumulated water that are stored in the mine pits, the accumulated water dissolves any harmful substances in the pits and then flows out through slope cracks or leftover abandoned roadways, which poses a very great threat to the underground and surface waters, as shown in Fig. [1](#page-1-0). With the increasing promotion of coal mine flling and mining technology, the demand for solid waste for use in mine backflling has also increased greatly. For example, coal gangue and fy ash are often used in mine backflling, but the annual gangue



<span id="page-1-0"></span>**Fig. 1** Diagram of groundwater pollution in a mining area

discharges only account for 10%–20% of coal production, and an insufficient supply of filling materials that is caused by long-term flling has inevitably become a problem (Wang et al. [2019a;](#page-11-0) [b;](#page-11-1) Fallgren et al. [2021](#page-10-0)).

China produces very large amounts of industrial byproduct gypsum each year. There are three main types of byproduct gypsum that are produced by industrial activities: titanium gypsum (TG), which is produced by neutralizing acidic liquid wastes with lime or calcium carbide slag during the production of sulfuric acid titanium dioxide; phosphorus gypsum (PG), which is produced by phosphorite that is eroded by sulfuric acid during the production of phosphoric acid; and fue gas desulfurization gypsum (FGDG), which is produced by removing the sulfur oxides in fue gas in most power plants in China by using the limestone gypsum method. In 2020, the total PG production was 74 Mt, which represented a yearly decrease of 1.3%, and the utilization rate was approximately 44%. The FGDG emissions from thermal power plants totaled approximately 73 Mt, which represented an increase of approximately 1%. TG emissions rank third, with an output of approximately 30 Mt, but their utilization rates were very low at approximately 8% (Yang [2021\)](#page-11-2). In response to the basic policy of green and lowcarbon recycling development to solve resource, environmental and ecological problems, gypsum is considered to be a flling material for mine backflling (Al Heib et al. [2010](#page-10-1); Li et al. [2020](#page-10-2), [2021;](#page-10-3) Zhang et al. [2017](#page-11-3), [2021](#page-11-4)), which not only provides an economic, safe and relatively environmentally friendly method for the large-scale disposal of solid waste but also promotes the waste-free and harmless green mining of mines. However, although the main component of the three types of gypsum is  $CaSO<sub>4</sub>·2H<sub>2</sub>O$ , they still contain impurities. When gypsum is used to fll the goaf of a coal mine and this occurs in an acidic or alkaline mine water environment for a long period, this increases the leaching of metal elements that are contained in the gypsum and will cause a risk of migration to the mine foor and could afect the groundwater.

A number of laboratory investigations of gypsum leaching have been reported in recent decades and have provided quantitative estimates of the amounts of toxic elements released. Wei et al.  $(2015)$  $(2015)$  used a  $H_2SO_4/HNO_3$  mixture, deionized water and seawater for leaching treatments. When seawater was used as the leaching medium, the heavy metal concentrations that were released from titanium gypsum were the largest, especially the Mn and Hg concentrations, which were 5.0 and 34.2 times those of deionized water, respectively. In addition, the leaching concentration of an  $H_2SO_4/HNO_3$  mixture as the leaching medium is also greater than that of deionized water, which indicates that TG has a strong ability to release heavy metals in solid–liquid leaching systems. When studying and analyzing the drainages, erosion gully waters and depression waters of a PG storage feld in the karst mountainous area of Guizhou, Wang et al. ([2019a,](#page-11-0) [b\)](#page-11-1) found that the concentrations of heavy metals such as Pb, Cd, Cr, As, and Hg exceeded Class III of the China Surface Water Environmental Standard (GB3838- 2002). Water standards, erosion and PG leaching that are caused by natural rainfall are the main reasons for heavy metal migration. Zhong et al. ([2018\)](#page-11-6) investigated the paddy soil within 50–200 m of a PG storage yard and found that the cadmium contents in the soil reached 1.14–2.86 mg/ kg, and the soil samples exceeded the soil environmental quality standard (GB15618–1995). Compared with TG and PG, the utilization rate of FGDG in China is the highest at approximately 80%. Although studies have shown that desulfurized gypsum can be used for mine backflling, the leakage risk of pollutant elements that affects the safety of the groundwater environment cannot be ignored, especially when the desulfurized gypsum is located in a water environment. Hao et al. ([2017\)](#page-10-4) indicated that 25% of total Pb, 77.4% of Mn, and 51.8% of Zn occurred as easily soluble forms in the FGD gypsum from Shanxi Province. Wang et al. [\(2017a](#page-11-7), [b](#page-11-8)) used the column leaching mode to conduct acid leaching experiments on two samples of FGDG from power plants in Wuhan and Zhejiang. The outputs exceeded the standard limit of Class V water quality in the Groundwater Quality Standard Water (GB/T 14848–93). The highest leaching amounts of Pb, As, Cr and Ni in the sample reached 3.92, 0.11, 0.2 and 0.47 mg/L, respectively, in the leaching medium with  $pH = 4.0$ , which exceeded the maximum allowable concentrations (e.g., 0.1 mg/L). Wang et al. ([2018\)](#page-11-9) pointed out that the current consumption of FGDG in China is usually relatively high at approximately 20–60 t/ hm<sup>2</sup>, which may lead to excessive accumulation of contaminated elements in soil within a few years if it is used in large quantities every year.

Yang et al. [\(2007\)](#page-11-10) considered that the contaminated elements in the fll material could penetrate into the aquifer through the mine foor rock layer via water seepage and difusion, which would cause permanent damage to the

groundwater environment. In their research on the migration of heavy metals, scholars have paid more attention to how heavy metal elements migrate in the soil and how they accumulate in rivers and other sediments. Tabelin et al. [\(2019](#page-11-11)) used a coal mine as the research object and analyzed the whole process of heavy metal elements from their release to entering the soil and fnally leaching into the groundwater and also established a heavy metal migration model. Jiang and Liang ([2007\)](#page-10-5) studied the heavy metal migration model in the saturated–unsaturated state and simulated the process of groundwater pollution of coal gangue leachates by using numerical calculations and laid a foundation for the study of pollutant migration patterns. Sui et al. ([2013\)](#page-11-12) studied the dispersibility and seepage characteristics of the unsaturated soil of a slag feld and simulated the migration of pollutants in the slag feld in unsaturated rock and a soil medium by using COMSOL Multiphysics software. This work indicates that COMSOL Multiphysics software can be used for pollutant migration simulation.

Based on the previous research foundation, the author found that (1) the types of gypsum in the industrial byproduct gypsum leaching experiment and the research conditions were relatively simple. (2) There are many studies on the use of industrial solid waste gypsum for mine backflling, but few studies have discussed the migration process during backflling of the metal elements contained in gypsum. Therefore, this study selects TG, PG, and FGDG as the research objects. In addition, the samples were placed in acidic, alkaline and deionized waters to analyze the leaching characteristics of the metal elements. At the same time, the coupling numerical simulation method of the seepage feld and concentration feld was established to explore the difusion characteristics and migration patterns of heavy metal elements when diferent types of gypsum were used as flling materials. This paper will further improve the theoretical system for recycling solid waste resources in mine flling work and has a certain degree of reference signifcance for protecting the groundwater environment.

## **2 Methods**

## **2.1 Gypsum samples**

The phosphorus gypsum, titanium gypsum and FGD gypsum used in the experiment were collected from a phosphate fertilizer plant, titanium powder plant and thermal power plant, respectively. All samples were dried in a 328 K oven for 19 h before the experiment and were then screened with

<span id="page-2-0"></span>**Table 1** Main chemical components of industrial waste gypsum

Chemical composi-	Mass fraction $(wt\%)$						
tion	FGDG	TG	PG				
MgO	0.3	0.155	0.055				
$\text{Al}_2\text{O}_3$	1.42	3.324	0.66				
SiO <sub>2</sub>	3.12	2.716	5.93				
SO <sub>3</sub>	44.62	40.27	53.7				
CaO	31.45	40.82	36.5				
Fe <sub>2</sub> O <sub>3</sub>	0.34	6.45	0.575				
$K_2O$	$\leq 0.4$	$\leq 0.1$	$\leq 0.4$				
ZrO <sub>2</sub>	$\leq 0.10$	$\leq 0.1$	$\leq 0.10$				
pН	8.9	8.3	5.0				

a 200 mesh for subsequent use. The main chemical components of the industrial waste gypsum are given in Table [1.](#page-2-0)

#### **2.2 Sequential batch extraction leaching**

The sequential batch extraction process is performed by regularly adding fresh leaching medium in the process of the leaching experiment to simulate the leaching conditions where the disposed gypsum experiences repetitive percolation of rainwater and/or acid mine drainage (AMD) solutions with low pH and the leachate coexists with the gypsum for a considerable period of time. The repetitive extractions help us to determine the highest concentrations of each constituent that are likely to leach out into natural environments (Dutta et al. [2009\)](#page-10-6).

In a typical run, 40 g of each of three gypsum samples were extracted with 200 mL of diluted  $H_2SO_4$  (pH = 1.8) and 3.1) for one week. The gypsum was separated from the extracting medium, and fresh diluted sulfuric acid was then added and the run continued for another week. The same procedure was repeated for four cycles. The leachate from each cycle was collected, the pH of the leachate was noted, and the trace elements in the leachate were analyzed. A series of experiments was performed by using the above procedure with NaOH solutions ( $pH = 10.4$  and 11.7).

The elemental concentrations (except As and Hg) in the leachates were determined by inductively coupled plasma emission spectrometry (ICP). The As and Hg concentrations in the leachates were estimated by using atomic fuorescence analysis (AFS).

## **2.3 Numerical simulation of heavy metal element migration**

Taking the working face of a mining area as the research background, the length of the working face is 120 m and is nearly horizontal, and the flling goaf and the coal seam floor constitute a system of upper and lower media. The mine floor consists of limestone with a thickness of 20 m, and the thickness of the flling area is 5 m. The model is divided into a free triangle mesh, and the mesh of the flling area is added to ensure the reliability of the results. The entire mesh consists of 2525 domain units and 265 side units. To better observe the migration of metal elements in the flling process, an observation point was defned at the middle line of the working face and at the center of the bottom of the flling area, with coordinates  $(60, -6)$ . The boundary labels of the model and the location of the observation point are shown in Fig. [2.](#page-3-0)

The subsurface fow module in the COMSOL Multiphysics software contains the most commonly used basic diferential equations and boundary conditions used in calculations of seepage fow. The Darcy equation model is a general seepage equation based on Darcy's law and the continuity equation of water fow. The expression is (Whitaker [1986\)](#page-11-13):

$$
\frac{\partial}{\partial t}(\rho \varepsilon) + \nabla \cdot \rho \left[ -\frac{k}{\mu} (\nabla p + \rho g \cdot \nabla D) \right] = Q_{\text{m}} \tag{1}
$$

where  $\epsilon$  is the porosity,  $\rho$  is fluid density (kg/m<sup>3</sup>), *k* is the permeability, $\mu$  is the fluid viscosity (Pa s),  $p$  is the pressure (Pa), *D* is the direction that represents vertical elevation (m), and  $Q<sub>m</sub>$  is the source item.

In addition, the equation that is used in this software to describe fuid fow in saturated unsaturated porous media is the Richards equation (Bear [2012](#page-10-7)):

$$
\rho \left( \frac{C_{\rm w}}{\rho g} + S_{\rm c} S \right) \frac{\partial p}{\partial t} + \nabla \cdot \rho \left[ -\frac{K_{\rm s}}{\mu} K_{r} (\nabla p + \rho g \cdot \nabla D) \right] = Q_{\rm m} \tag{2}
$$

where,  $C_w$  is water capacity; $S_c$  is effective saturation (dimensionless); $S_c = (\theta_s - \theta_r)/(1 m \cdot \rho g)$ , where  $\theta_s$  and  $\theta_r$  denote the volume fractions of the fuid at saturation and after drainage, respectively; *S* is a storage coefficient  $(1/m)$ ;  $K<sub>s</sub>$  is saturated permeability; and  $K_r$  is relative permeability.

Assuming that the fuid experiences seepage motion only under the action of gravity, it conforms to Darcy's law of motion (Huang et al. [2014](#page-10-8)):

$$
u = -\frac{k}{\mu} \nabla p \tag{3}
$$

where u is the fluid seepage velocity vector  $(m/s)$ .

During the process of pollutant migration, both molecular difusion and mechanical dispersion follow Fick's frst law, and these two effects occur at the same time. Because dispersion and diffusion are difficult to distinguish, the two are generally referred to as the hydrodynamic dispersion coefficient, and the hydrodynamic dispersion equation is written as follows (Bachmat and Bear [1964](#page-10-9)):

$$
\frac{\partial}{\partial x}\left(D_h \frac{\partial C}{\partial x}\right) - \frac{\partial}{\partial x}(uC) = \frac{\partial C}{\partial t}
$$
(4)

where  $D<sub>h</sub>$  is the hydrodynamic dispersion coefficient.

#### **2.4 Initial values and boundary conditions**

Assuming that the goaf is full of water, the gravitational potential energy of the mine water produces a pressure head on the foor. Combined with the experimental results of the metal element release patterns in gypsum, Zn is taken as an example for the numerical simulation. The initial value of the infow concentration is the fnal leaching concentration of Zn when deionized water is used as the leaching medium. The boundary conditions and governing equations are shown in Tables [2](#page-4-0) and [3,](#page-4-1) respectively.



<span id="page-3-0"></span>**Fig. 2** Mine flling numerical subdivision model



<span id="page-4-0"></span>

Richards' equation (dl) Pressure head 6,8 $H_{\rm p} = \frac{p}{\rho g}$	Boundary label	
$-n \cdot \rho u = 0$ 1, 2, 3, 5, 10, 11, 12 No flow		
1,3,5,10,11,12 Transport of diluted species in No flux $-n \cdot J_i = 0$		
porous media (tds) Inflow 6,7,8 $c_i = c_{0,i}$		
$n \cdot D_i \nabla c_i = 0$ Outflow		

<span id="page-4-1"></span>**Table 3** Parameters of floor in the model



## **3 Results**

# **3.1 Sequential batch extraction**

## **3.1.1 Changes in pH of the leachate**

The time evolution of the leachate pH values for diferent leaching media (e.g., diluted  $H_2SO_4$  pH = 1.8 and 3.1; deionized water; diluted NaOH  $pH = 10.3$  and 11.7) at solid-liquid ratios of 1:5 is shown in Fig. [3](#page-4-2). Leaching was conducted





<span id="page-4-2"></span>**Fig. 3** Time evolution of the leachate pH during sequential batch extraction

in 4 cycles spanning a seven-day period. During the repeated contact of gypsum with the leaching medium, the leachate pH values change accordingly.

Most of the PG leachate is strongly acidic, especially the PG leachate in the frst cycle, which is most acidic, with a pH range of 1.49–4.49, which indicates strong acidity, probably because both alkaline and acidic leaching media can efectively leach out the residual acidic substances in phosphorus gypsum (Chen and Mao [2007](#page-10-10)). As the time and pH of the leaching medium increase, the pH values of the leachate increased accordingly, especially under deionized water and NaOH, and the pH of the fourth cycle leachate reached a range of 5.32–6.87. However, the pH change of the leachate was not obvious when it was leached under  $H_2SO_4$  (pH = 1.8 and 3.1), and the values at the end of the experiment were 1.56 and 3.01, respectively, and when compared with the initial pH values, only increased by 0.7 and 1.04, respectively, which indicate that the leachate pH under strong acidic conditions did not change over time (Fig. [3a](#page-4-2)). The pH changes of the FGD and titanium gypsum leachates exhibited obvious efects over time. Figure [3](#page-4-2)b shows that the pH range of the FGDG leachate in the  $H_2SO_4$  leaching medium is 5.19–7.18, which neutralizes the acidity of  $H_2SO_4$ and may be due to the alkalinity of FGD itself. When NaOH is used as the leaching medium, the pH values of the leachate are lower than the initial pH of the leaching medium even under alkaline conditions, which may be due to the  $Ca^{2+}$  ions that are released by FGDG that replace the Na<sup>+</sup> ions in NaOH, which thus decreases the pH (Wang et al. [2017a](#page-11-7), [b](#page-11-8)). The pH values of the leachates obtained from TG in acidic or alkaline leaching media over time are similar to those of the deionized water leachate. In the frst period, the pH values were in the range of 4.71–5.23, and the pH values of the second cycle reached 7.48–11.05, which were the peak values among the four cycles; then, the pH exhibited a small decrease. This is because TG has a good bufer efect and can maintain pH stability. Therefore, even under the diferent leaching media conditions, the pH levels of the leachate did not show large diferences.

#### **3.1.2 Leaching of metal elements**

Figure [4](#page-6-0)a, d show that the leaching characteristics of Zn and Mn in PG were relatively similar. The leaching concentrations of the metal elements decreased with increasing pH (except for deionized water). At  $pH = 11.7$ , the released metal element concentrations were the smallest, which shows that alkaline conditions are not conducive to the leaching of metal elements in phosphorus gypsum, which may be caused by the formation of phosphate precipitates of the metal elements under alkaline conditions (Brückner et al. [2020](#page-10-11)). During the release process of Mn, the concentration that was released in the leaching medium with an initial pH of 1.8 was the largest, which reached 0.073 and 3.3 mg/L, which was followed by deionized water, and the concentrations in both of these media were very similar. During the Zn release process, the concentration at  $pH = 1.8$  was the largest only in the frst cycle. From the second cycle to fourth cycle, the released concentrations were the largest when deionized water was used as the leaching medium. Furthermore, the concentrations of the leached metal elements gradually decreased under all conditions, and the concentration was close to 0 in the fourth period. This indicates that when PG is exposed to acidic solvents (such as acid rain or acidic mine water) or nonacid precipitation, this will promote the release of the metal elements in phosphorus gypsum and the released metal element concentrations gradually decrease during repeated contact.

The Zn concentrations released by TG in NaOH ( $pH =$ 10.3 and 11.7) were greater than those in  $H_2SO_4$  (pH = 1.8) and 3.1), and the leachate was in a weakly alkaline state from the second cycle onward (Figs. [3,](#page-4-2) [4](#page-6-0)b). Although the acidic leaching medium can consume the alkalinity of TG itself, the pH decreases slowly, and the release of metal elements under low pH conditions is less obvious. This phenomenon can be explained as the result of the buffering effect of titanium gypsum on the acidity, which is similar to the conclusion obtained by Wei et al. ([2015\)](#page-11-5). Figure [4e](#page-6-0) shows the pattern of change for the Mn leaching concentrations in TG. Except for the leaching medium with an initial pH of 1.8, the leaching concentrations of Mn under other conditions were quite low and were even below the detection limit. This may be because the leachate pH in the frst cycle was in the range of 4.71–5.23, which represents weakly acidic conditions. Thus, the acidic conditions had certain efects on the release of the metal elements in TG. Then, with increasing pH, the Mn concentrations signifcantly decreased. When extracting Mn from gypsum with a leaching medium of pH = 11.7, only very small amounts of Mn were released in the frst cycle, and the concentrations in later cycles were below the detection limit. This result may be because Mn is in a weakly alkaline condition in the form of oxyhydroxide, or hydroxide precipitates, or is adsorbed in the solid phase (Neculita and Rosa [2019\)](#page-10-12), which results in extremely small amounts present in the leachate that can even be lower than the detection limit.

Figure [4](#page-6-0)c, f show that the metal elements in FGDG were more easily released in the low pH leaching medium. The leaching concentration changes for Zn and Mn were similar; both were liable to be leached under acidic conditions, and the concentrations under each condition gradually decreased and became stable with the extension of time. The release concentrations of Zn and Mn were the largest in  $H_2SO_4$  (pH  $= 1.8$ ) because FGDG has more impurities and its structure is relatively loose (Lei et al. [2017\)](#page-10-13). For initial pH values of 1.8 and 3.1, higher concentrations of  $H^+$  will destroy the



<span id="page-6-0"></span>**Fig. 4** Leaching concentrations of Zn in PG (**a**), TG (**b**) and FGDG (**c**); leaching concentrations of Mn in PG (**d**), TG (**e**) and FGDG (**f**)

structure of FGDG so that the metal elements are replaced by the  $H<sup>+</sup>$  ions in the gypsum particles and dissolve into a water phase. Under initial pH conditions of 10.3 and 11.7, the leaching amounts of Mn in FGDG were extremely low. The Mn concentrations were all lower than the detection limit during the entire leaching process at NaOH ( $pH =$ 11.7), which may be due to the presence of Mn in the form of precipitates under strong alkaline conditions. However, Zn is still released under strong alkaline conditions, probably because Zn combines with hydroxyl groups to form soluble substances, which will be leached in strong alkaline leaching media (Kim and Hyun [2015](#page-10-14)).

According to the leaching tests of the three gypsum types under diferent leaching media conditions, the maximum leaching amounts of their pollutant elements were compared with the national environmental quality standards, with the details shown in Tables [4,](#page-7-0) [5](#page-7-1) and [6](#page-7-2). Although the leaching contents of the heavy metal elements in the three gypsum types are all lower than those specifed in the Identifcation Standards for Hazardous Wastes Identifcation for Extraction

Elements	Leachable contents of PG (mg/L)					GB5085.3-2007	GB8978-1996	GB/T1484–93 limited value		
	Deionized water $pH = 1.8$ $pH = 3.1$			$pH = 10.3$	$pH = 11.7$	limited value (mg/L)	limited value (mg/L)	(mg/L)		
								III	<b>IV</b>	V
As	0.378	0.399	0.36	0.354	0.347	5	0.5	$\leq 0.05$	$\leq 0.05$	> 0.05
Hg	0.0117	0.00547	0.0101	0.00956	0.00365	0.1	0.05	${}_{0.001}$	${}_{0.001}$	> 0.001
C <sub>d</sub>	0.074	0.082	0.067	0.06	0.035		0.1	$\leq 0.01$	$\leq 0.01$	> 0.01
Cr	0.16	0.25	0.15	0.11	ND	15	1.5	$\leq 0.05$	$\leq 0.1$	> 0.1
Pb	0.31	0.36	0.26	0.21	ND	5		${}_{0.05}$	$\leq 0.1$	> 0.1
Zn	2.79	3.07	2.53	2.28	0.733	100	$2.0 - 5.0$	< 1.0	$\leq 5.0$	> 5.0
Mn	17.9	18.6	15.4	14.8	12	NG	$2.0 - 5.0$	$\leq 0.1$	$\leq 1.0$	> 0.1
pH	2.05	1.49	1.97	2.08	4.49	NG	$6 - 9$	$6.5 - 8.5$	$5.5 - 6.5$ $8.5 - 9$	< 5.5 > 9.0

<span id="page-7-0"></span>**Table 4** Comparison between the leachable contents of the elements in PG gypsum and the national environmental quality standard limits for hazardous pollutants

"ND" represents "not detected"; "NG" represents "not given"

<span id="page-7-1"></span>**Table 5** Comparison between leachable contents of the elements in TG gypsum and national environmental quality standard limits for hazardous pollutants

Elements	Leachable contents of TG (mg/L)					GB5085.3-2007	GB8978-1996	GB/T14848–93 limited value		
	Deionized water $pH = 1.8$ $pH = 3.1$			$pH = 10.3$	$pH = 11.7$	limited value (mg/L)	limited value (mg/L)	(mg/L)		
								Ш	<b>IV</b>	V
As	0.0014	0.0007	0.001	0.0016	0.0129	5	0.5	$\leq 0.05$	$\leq 0.05$	> 0.05
Hg	$4E-5$	ND	ND	ND	ND	0.1	0.05	${}_{0.001}$	$\leq 0.001$	> 0.001
C <sub>d</sub>	ND	0.008	0.005	ND	ND		0.1	$\leq 0.01$	$\leq 0.01$	> 0.01
Cr	ND	0.05	0.03	ND	ND	15	1.5	$\leq 0.05$	$\leq 0.1$	> 0.1
Pb	ND	ND	ND.	ND	ND	5		$\leq 0.05$	$\leq 0.1$	> 0.1
Zn	0.013	0.02	0.015	0.033	0.031	100	$2.0 - 5.0$	$\leq 1.0$	$\leq 5.0$	> 5.0
Mn	0.144	0.983	0.239	0.12	0.004	NG	$2.0 - 5.0$	< 0.1	$\leq 1.0$	> 0.1
pH	4.82	5.23	4.96	4.76	4.71	NG	$6 - 9$	$6.5 - 8.5$	$5.5 - 6.5$ $8.5 - 9$	< 5.5 > 9.0

"ND" represents "not detected"; "NG" represents "not given"

<span id="page-7-2"></span>**Table 6** Comparison between leachable contents of the elements in FGD gypsum and national environmental quality standard limits for hazardous pollutants

Elements	Leachable contents of FGD (mg/L)					GB5085.3-2007	GB8978-1996	GB/T14848–93 limited value		
	Deionized water $pH = 1.8$ $pH = 3.1$ $pH = 10.3$				$pH = 11.7$	limited value (mg/L)	limited value (mg/L)	(mg/L)		
								IΠ	IV	V
As	ND	0.0005	0.0003	ND	ND	5	0.5	$\leq 0.05$	$\leq 0.05$	> 0.05
Hg	ND	ND	ND	ND	ND	0.1	0.05	${}_{0.001}$	${}_{0.001}$	> 0.001
C <sub>d</sub>	ND	0.006	ND	ND	ND		0.1	$\leq 0.01$	${}_{0.01}$	> 0.01
Cr	0.03	0.08	0.05	ND	ND	15	1.5	$\leq 0.05$	$\leq 0.1$	> 0.1
Pb	ND	0.07	ND	ND	ND	5		$\leq 0.05$	$\leq 0.1$	> 0.1
Zn	0.022	0.073	0.046	0.033	0.038	100	$2.0 - 5.0$	$\leq 1.0$	$\leq 5.0$	> 5.0
Mn	1.78	3.3	1.97	0.281	ND	NG	$2.0 - 5.0$	$\leq 0.1$	$\leq 1.0$	> 0.1
pH	5.22	5.37	5.19	5.3	5.42	NG	$6 - 9$	$6.5 - 8.5$	$5.5 - 6.5$ $8.5 - 9$	< 5.5 > 9.0

"ND" represents "not detected"; "NG" represents "not given"

Toxicity (GB 5085.3–2007), gypsum is not classifed as hazardous solid waste, but the infuence of leached heavy metal elements on groundwater quality cannot be ignored. The maximum leaching amounts of the pollutant elements in PG exceed the limit defned in the Quality Standards for Ground Water (GB/T 1484–93) Class III water quality standard. The maximum leaching concentrations of Hg, Cd, Cr, Pb, and Mn reached 0.0117, 0.082, 0.25, 0.36, and 18.6 mg/L, respectively, which all exceeded the limits of the Class V water quality standards. The maximum Mn concentration from TG exceeded the limit defned in the groundwater quality standard V class water quality standard. When the leaching media consisted of deionized water,  $H_2SO_4$  (pH = 1.8,  $pH = 3.1$ ) and NaOH ( $pH = 10.3$ ), the Mn concentrations were 0.144, 0.983, 0.239, and 0.12 mg/L, respectively. The leaching results for FGDG are similar to those of TG. When the leaching media consisted of deionized water,  $H_2SO_4$  (pH  $= 1.8$ , pH  $= 3.1$ ) and NaOH (pH  $= 10.3$ ), the Mn concentrations exceeded the groundwater quality standard V water limit and were 1.79, 3.3, 1.97, and 0.281 mg/L, respectively. It is worth noting that the limit defned in the Class III water quality standard is based on the human health benchmark value, and water is not suitable for drinking if it exceeds the limits of Class IV and V water quality standards.

#### **3.2 Numerical simulation result analysis**

COMSOL Multiphysics software was used to simulate the migration and difusion of the leached metal elements in the mine floor when PG, FGDG and TG were used as the filling materials, and the concentration distributions of Zn from the diferent gypsum samples at 10a, 100a and 200a were obtained, as shown in Fig. [5.](#page-8-0) At the same time, to facilitate the analysis of the metal element concentration distributions and migration and difusion changes, curves of the concentration distributions of Zn at the observation point with the passage of time and the increase in distance along the mine floor direction were drawn, as shown in Figs. [6](#page-9-0) and [7](#page-9-1).

According to Fig. [5,](#page-8-0) for the diferent gypsum types, the concentration distributions of the metal elements and the migration distances exhibited signifcant changes over time. According to the cloud charts, the migration distances for PG, FGDG and TG at 10a were 1.8, 1.6 and 1.2 m, respectively. Figure [7](#page-9-1) shows that the Zn migration distances at 200a were analyzed in detail, and the migration distances for PG, FGDG and TG reached 8.2, 8.1 and 7.5 m, respectively. When flling with diferent gypsum contents, the Zn concentration distributions were signifcantly diferent, which were caused by the diferent initial concentrations. When the flling body of the goaf consisted of PG, the initial concentration of the leached metal elements was greater than those of the other two gypsum types, which thus afected the concentration distribution range of the metal



<span id="page-8-0"></span>**Fig. 5** Cloud maps of the Zn concentration distributions at 10a, 100a and 200a  $(10^{-5} \text{ mol/L})$ 

elements. In addition, it can also be found that in all cases, the metal element concentrations near the flling area were the greatest, and the difusion ability of the metal elements decreased with increasing depth, which are similar to the results obtained by Song et al. [\(2018](#page-11-14)).

Figure [6](#page-9-0) shows that during the flling processes of the three gypsum materials, the Zn concentrations gradually increased with time. When titanium gypsum was used as the flling material, the Zn concentrations changed most



<span id="page-9-0"></span>**Fig. 6** Zn concentration distribution curves at the observation point over time  $(10^{-5}$  mol/L)

slowly, while when phosphorus gypsum and FGD gypsum were used as the flling materials, the changes in Zn concentrations were relatively obvious. The PG and FGDG concentrations increased the fastest during the initial period of 0–25a, which indicated that the metal elements in the PG and FGDG difused most rapidly in the mine foor at the early stage and then gradually stabilized. The order of the concentration change rates is PG > FGDG > TG, and the Zn concentrations in the three materials at the end of the simulation are  $2.14 \times 10^{-4}$ ,  $1.57 \times 10^{-4}$  and  $4.46 \times 10^{-5}$  mol/L. These results show that the difusion rates and concentration distribution changes of the elements are afected by their initial concentrations.

Figure [7](#page-9-1) shows that during the gypsum flling process, the metal element concentrations all exhibited downward trends, especially for the cases of phosphorus gypsum and FGD gypsum. The Zn concentration distributions from the diferent gypsum samples exhibited signifcant diferences along the depth direction of the mine floor from 0 to 6 m and at approximately 6 m and deeper, the diferences in the Zn concentration distributions began to decrease. As shown on the right part of Fig. [7,](#page-9-1) the concentration distribution at 4–10 m is enlarged, and it can be observed that there are generally no diferences in the migration distances of the metal elements for the three gypsum types after 8.2 m. Therefore, due to the diferences in the initial metal element concentrations, the concentration distributions and migration distances of the elements in the migration and difusion processes of the bottom plate are diferent, among which the changes in concentration distributions and element difusion rates were the largest in the initial stage, and the diferences among the diferent gypsum types gradually decreased in the later stage. The maximum Zn migration distances from PG, FGDG and TG in the mine floor reached 8.2, 8.1 and 7.5 m, respectively.

# **4 Conclusions**

(1) During the process of repeated contact of the three types of industrial waste gypsum with the leaching medium, the pH changes accordingly, and the pH changes will afect the leaching patterns of the heavy metal elements in gypsum. The pH levels of the PG leachate are low in both alkaline and acidic environments, which range from 1.49 to 4.49. In the  $H_2SO_4$  $(pH = 1.8)$  leaching medium, the Zn and Mn release concentrations were the highest, which were 3.07 and 18.6 mg/L, respectively, while in NaOH ( $pH = 11.7$ ), the Zn and Mn release concentrations were the lowest. The leaching medium of NaOH ( $pH = 10.3$  and 11.7) was not conducive to the release of harmful elements from PG. FGDG can efectively neutralize the acidity and alkalinity of the leaching medium. Moreover,



<span id="page-9-1"></span>**Fig. 7** Zn concentration distributions at diferent depths along the mine foor direction at 200a (10−5 mol/L)

the metal elements in FGDG were easier to leach. In  $H_2SO_4$  (pH = 1.8), the Zn and Mn release concentrations were 0.073 and 3.3 mg/L, respectively. With increasing leaching times, the metal element concentrations for each condition gradually decrease and then tend to become stable. There were no signifcant differences in the pH values of the TG leachate under the diferent conditions. Because TG has a bufering efect on the acidity, the metal element releases are not obvious when the leaching medium is  $H_2SO_4$  (pH = 1.8 and 3.1).

- (2) According to the concentrations of metal elements that were leached from the three gypsum types, it can be judged that they are not classifed as hazardous solid wastes, but whether they pose a risk to the groundwater environment when they are used as mine flling materials cannot be ruled out. The maximum concentrations of the heavy metals elements leached from PG exceed the limits of the Class III water quality standards for ground water. Among them, the maximum leaching concentrations for Hg, Cd, Cr, Pb, and Mn reached 0.0117, 0.082, 0.25, 0.36, and 18.6 mg/L, respectively, which exceeded the limits defned in the Class V water quality standard. The maximum leaching amounts of Mn from TG and FGDG also exceeded the limits defned in the Class V water quality standard.
- (3) When the three types of gypsum were used as flling materials, the concentration distributions and migration distances of the metal elements exhibited signifcant changes over time. However, the concentration distributions, difusion rates and migration distances in the mine foor of the metal elements from diferent gypsum types are afected by the initial concentrations. The concentration distribution changes and element diffusion rates were largest in the early stage, and the differences among the diferent gypsum types gradually decreased in the later stage. These were ranked as PG > FGDG > TG. Furthermore, the fnal Zn concentrations that were leached from PG, FGDG and TG were 2.14  $\times$  10<sup>-4</sup>, 1.57  $\times$  10<sup>-4</sup> and 4.46  $\times$  10<sup>-5</sup> mol/L, respectively. The maximum Zn migration distances from PG, FGDG and TG in the mine floor were 8.2, 8.1 and 7.5 m, respectively.

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